



Coadvise + Treasure programmes  
Specialist Course  
Tlemcen, 7<sup>th</sup> - 11<sup>th</sup> February 2010

 POLITECNICO DI MILANO



**Biomass activity measurements**

**Part 2 - Respirometry and  
Titrimetry**

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# General Index (2)

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- 1) Fundamentals of Microbiology (*short hints*)
- 2) Main microbial substrates in wastewater: organic substances and nitrogen compounds
- 3) Bacterial activity assessment techniques**
  - **Respirometry**
  - **Titrimetry**
  - Manometry
  - Calorimetry



Bacterial activity can be evaluated in batch tests by tracking:

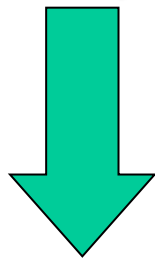
- The concentration of a substrate/product by:
  - manual sampling and analysis
    - ✓ 😊 simple and conventional
    - ✓ 😞 time consuming
  - using an on-line probe: titrimetry / respirometry
    - ✓ 😊 simple and convenient
    - ✓ 😞 dependent on probe availability/stability/reliability
  - measuring reaction by-products: manometry (gas production) and calorimetry (heat exchanged)
    - ✓ 😊 simple and convenient
    - ✓ 😊 simple and convenient (on-line data)
    - ✓ 😞 dependent on instrument reliability/sensitivity



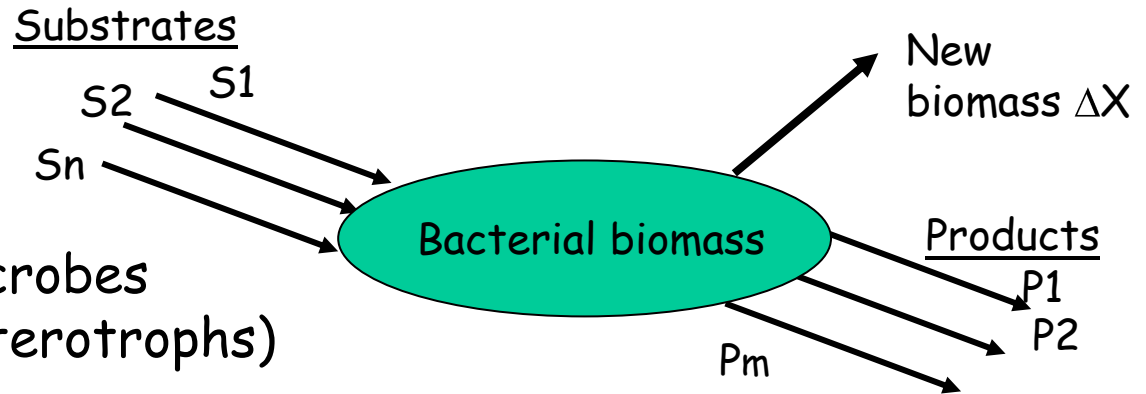
# RESPIROMETRY



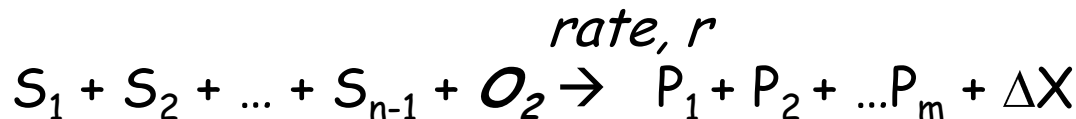
*Technique that draws information about aerobic biological reactions through the analysis of the oxygen consumption rate*



Applicable to aerobic microbes (both autotrophs and heterotrophs)



Under *aerobic conditions*, one of the substrates is dissolved oxygen ( $O_2$ , which acts as electron acceptor) :



**reaction rate,  $r$** , is proportional to consumption rate of oxygen:

$$r \propto r_{O_2} = d(O_2)/dt$$

Respirometry can be used to estimate:

## 1. Biomass growth kinetic and stoichiometric parameters such as:

- ✓ maximum growth rate ( $\mu$ ,  $d^{-1}$ )
- ✓ decay rate ( $b_h$ ,  $d^{-1}$ )
- ✓ half-saturation constant ( $K_s$ )
- ✓ cell yield coefficient ( $Y$ )

$$-\frac{dS_O}{dt} = \hat{\mu}_H \cdot \left( \frac{S_S}{S_S + k_S} \right) \cdot \left( \frac{S_O}{S_O + k_{OH}} \right) \cdot X_{BH} \cdot \frac{1 - Y_H}{Y_H} + \hat{\mu}_A \cdot \left( \frac{S_{NH}}{S_{NH} + k_{NH}} \right) \cdot \left( \frac{S_O}{S_O + k_{OA}} \right) \cdot X_{BA} \cdot \frac{4,57 - Y_A}{Y_A}$$

## 2. Organic substrate characteristics :

- ✓ Rapidly biodegradable fraction (rbCOD,  $mg L^{-1}$ )
- ✓ Slowly biodegradable fraction (sbCOD,  $mg L^{-1}$ )
- ✓ Toxicity and growth inhibition (fraction of  $\mu_{max}$ )

A **RESPIROMETER** measures oxygen concentration vs time and is capable of deriving the oxygen consumption rate ( $dO_2/dt$ ). The output of a respirometer is a **RESPIROGRAM**

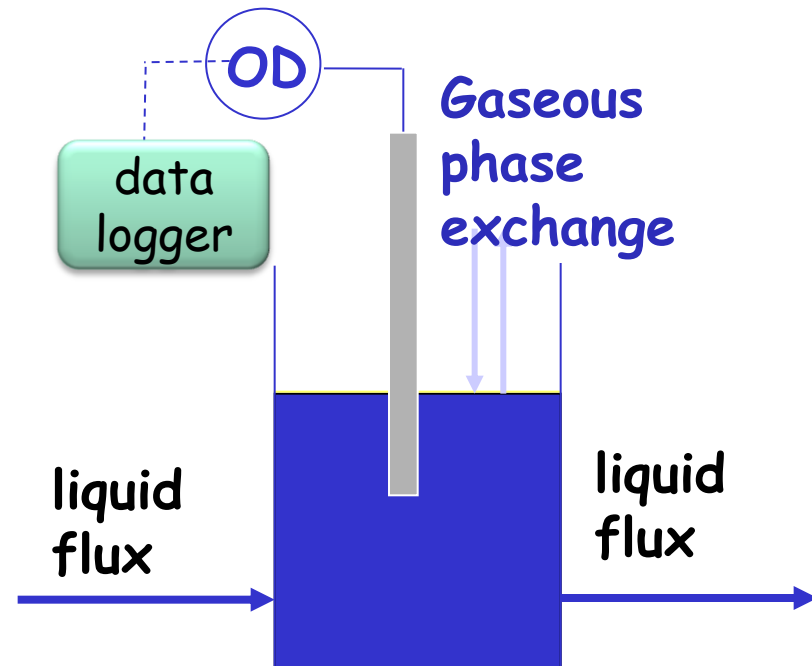
i.e.: graph of Oxygen Uptake Rate ( $r_o$ , or OUR,  $mgO_2 L^{-1} h^{-1}$ ) vs time

Once the concentration of VSS is known, then a specific OUR can be calculated ( $sOUR$ ,  $mgO_2 gVSS^{-1} h^{-1}$ )

A respirometer is made of:

- A biological reactor (vessel)
- An  $O_2$  concentration measuring probe
- A data acquisition and logging system

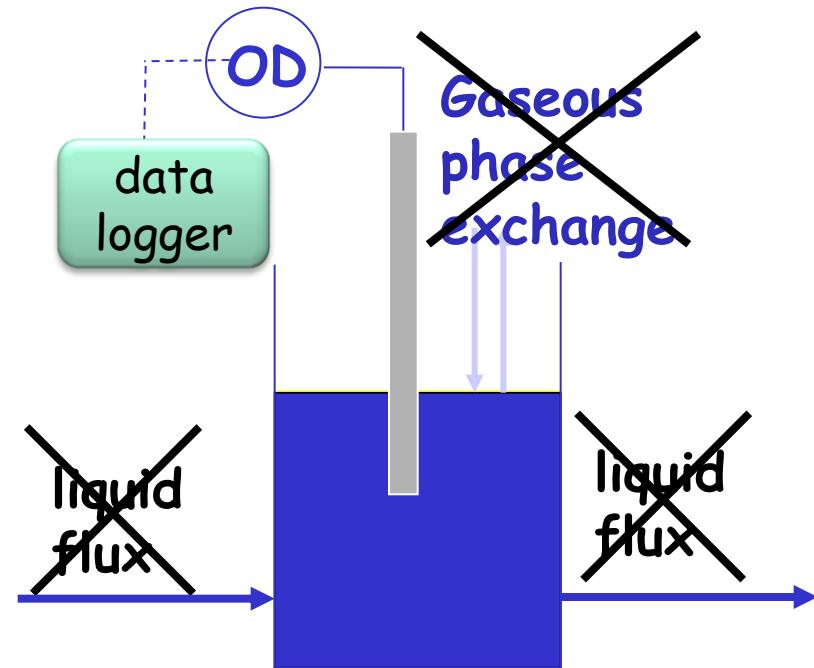
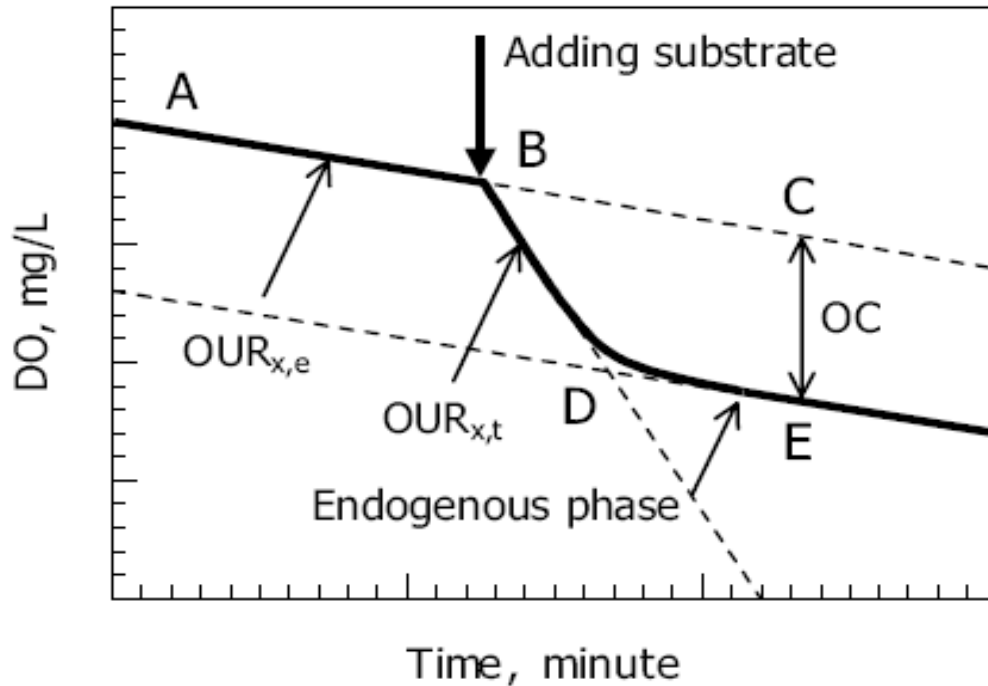
Oxygen can be measured in the gas phase or, more commonly, in the liquid phase





## CLOSED RESPIROMETER

batch reactor - neither liquid, nor gaseous flux  $\rightarrow$  Oxygen variation is due to biological consumption only

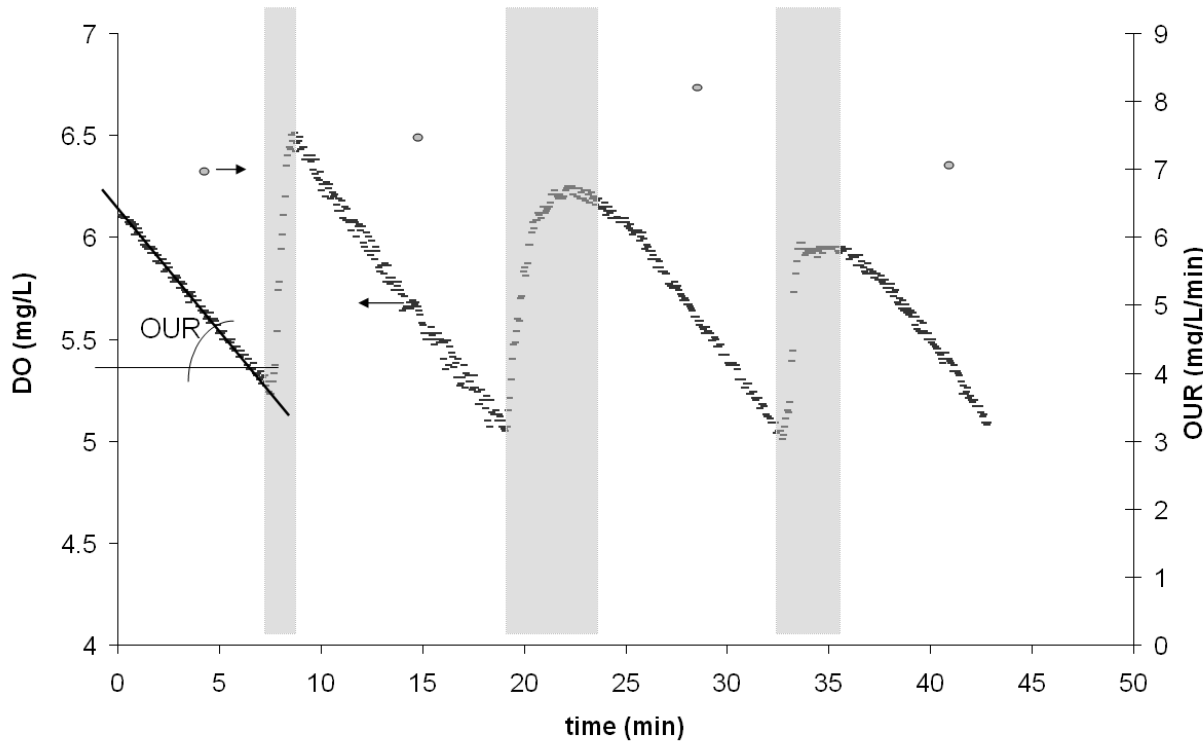






## OPEN RESPIROMETER

Oxygen is not limiting: periodic aeration starts as  $O_2$  concentration falls below a pre-set limit



OUR is determined as the slope during non-aerated periods



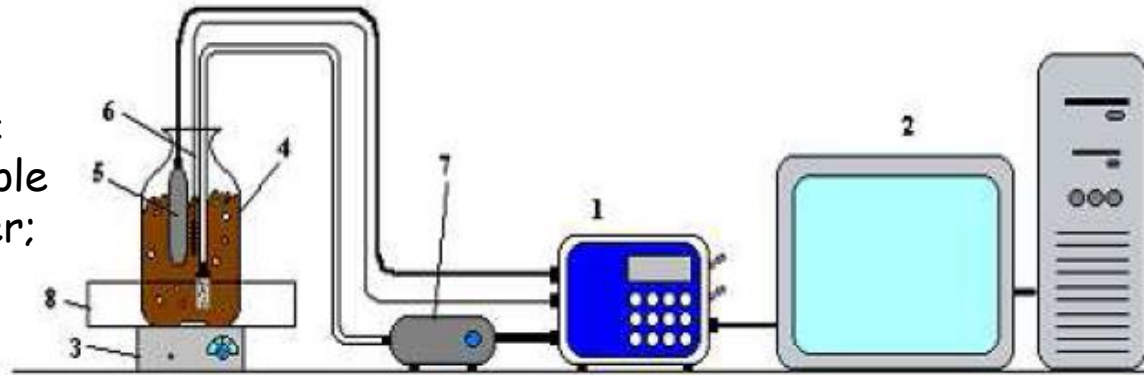
# Respirometry (6): respirometer and respirograms

## - OUR analysis (1)

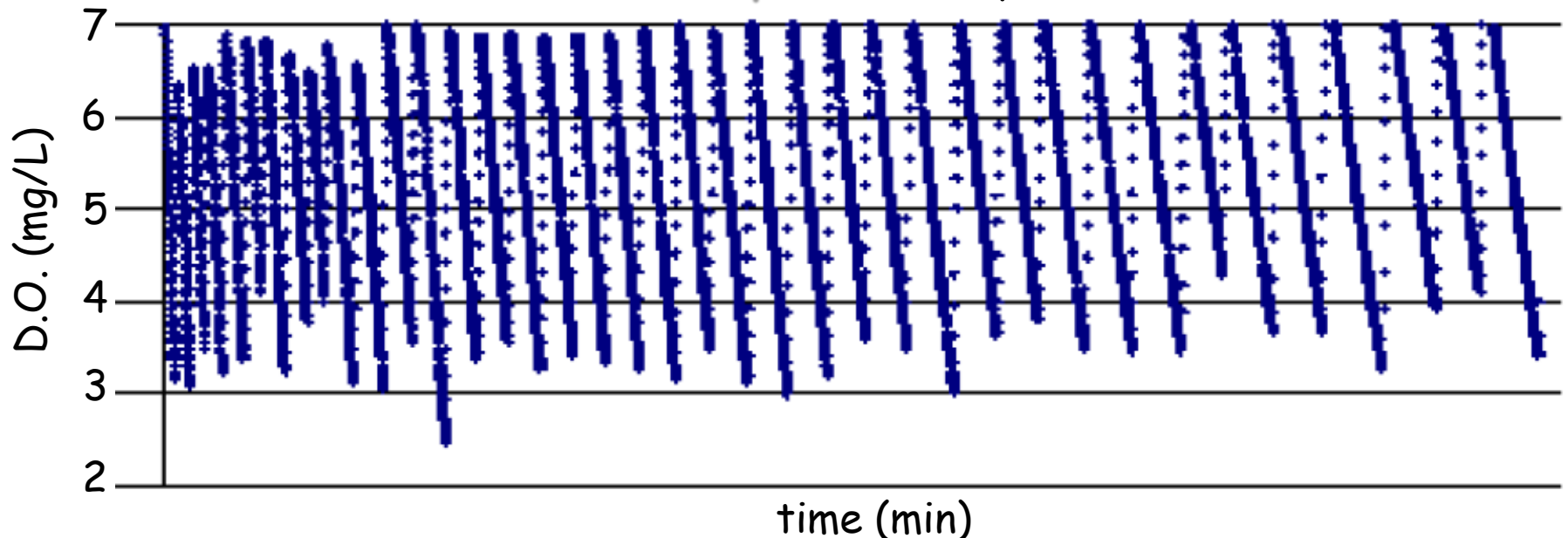
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### A Lab respirometer:

1: DO recorder; 2: PC; 3: magnetic stirrer; 4: Serum bottle with sample and activated sludge ; 5: DO-meter; 6: aerator (porous stone); 7: air compressor; 8: thermostatic bath



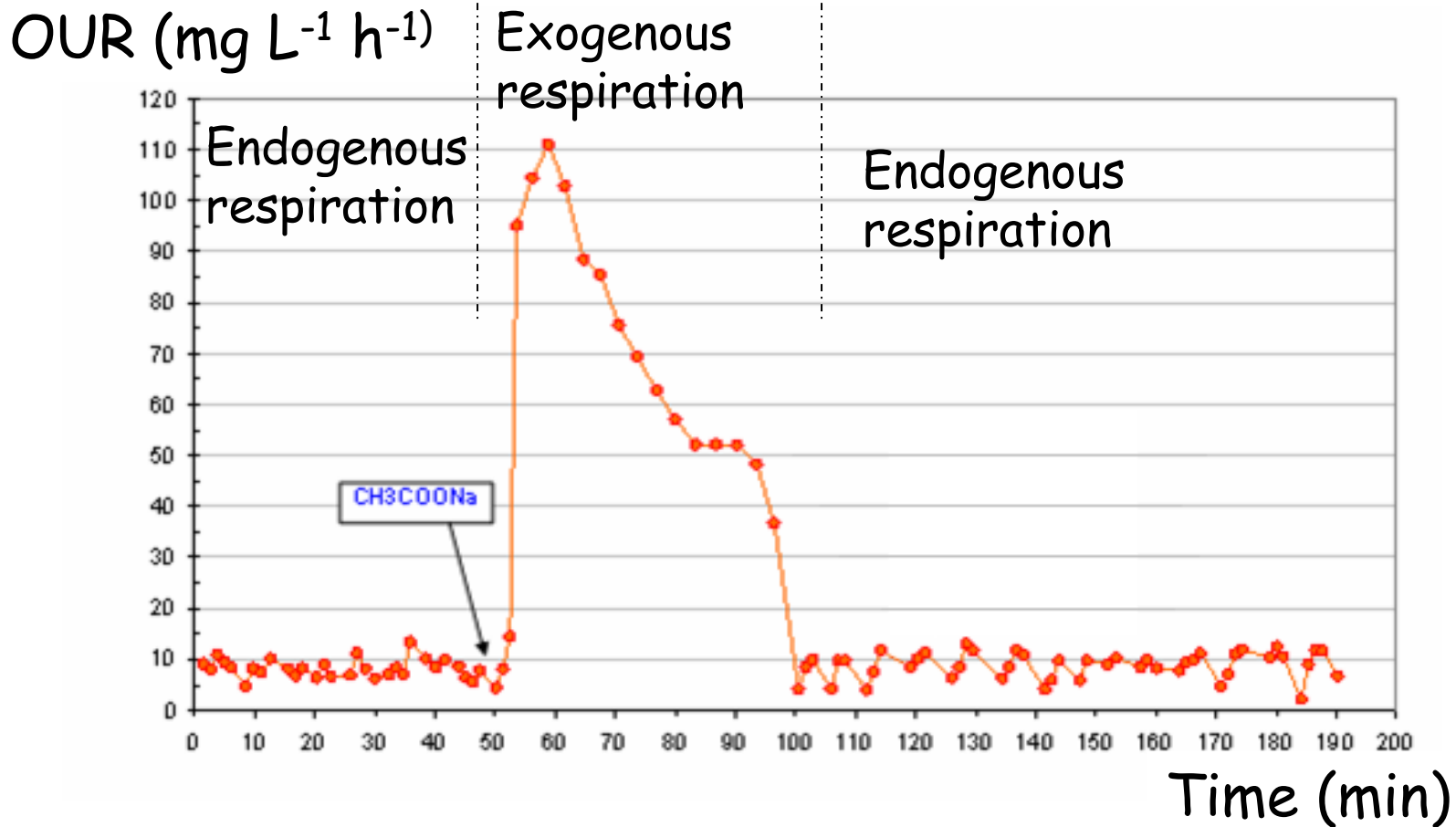
raw D.O. measurements: **respiration** (slopes) and re-aeration





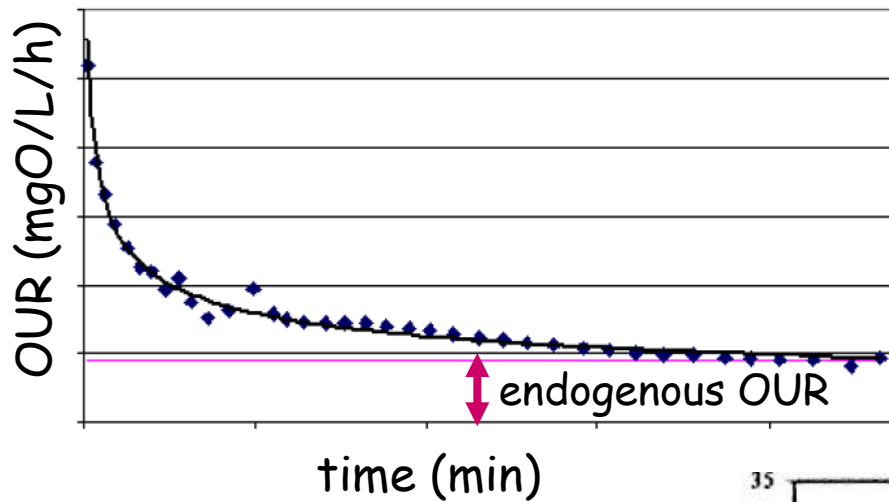
# Respirometry (7): respirometer and respirograms - OUR analysis (2)

Example of respirogram: acetate (rbCOD) is added to an activated sludge sample





# Respirometry (8): respirometer and respirograms - OUR analysis (3)

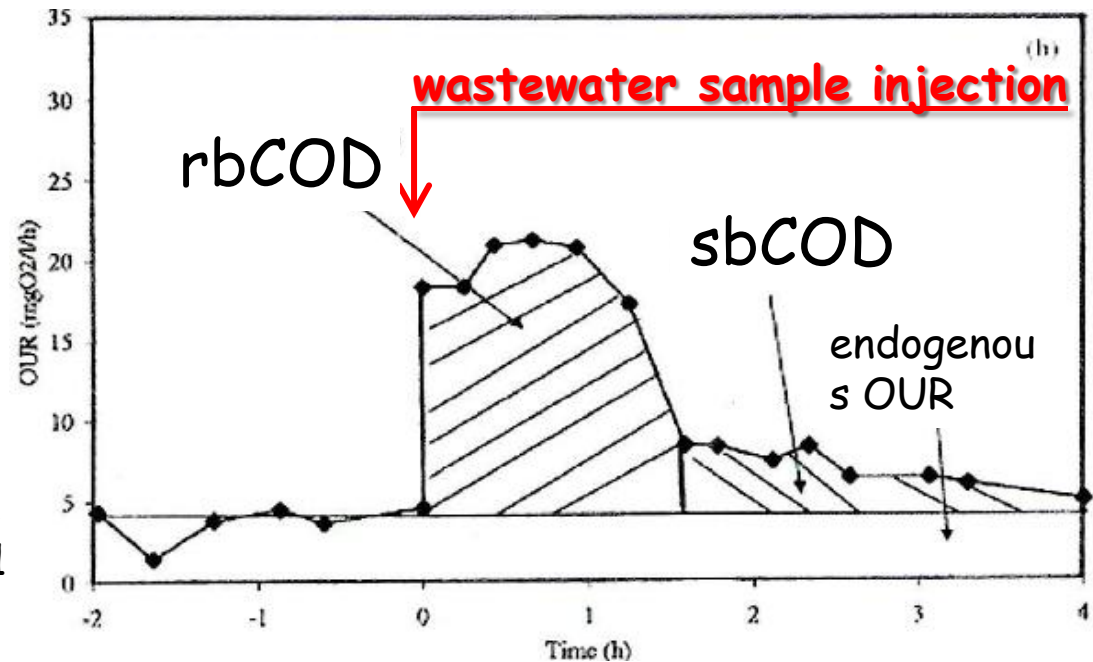


## OUR chart (respirogram)

each point is the value of "1 slope" taken from the raw data in the previous graph

## OUR chart (respirogram)

for the determination of rbCOD and sbCOD; care must be taken to choose the right F/M ratio (usually  $F/M = 0,1$  to  $0,2$  gCOD/gVSS)



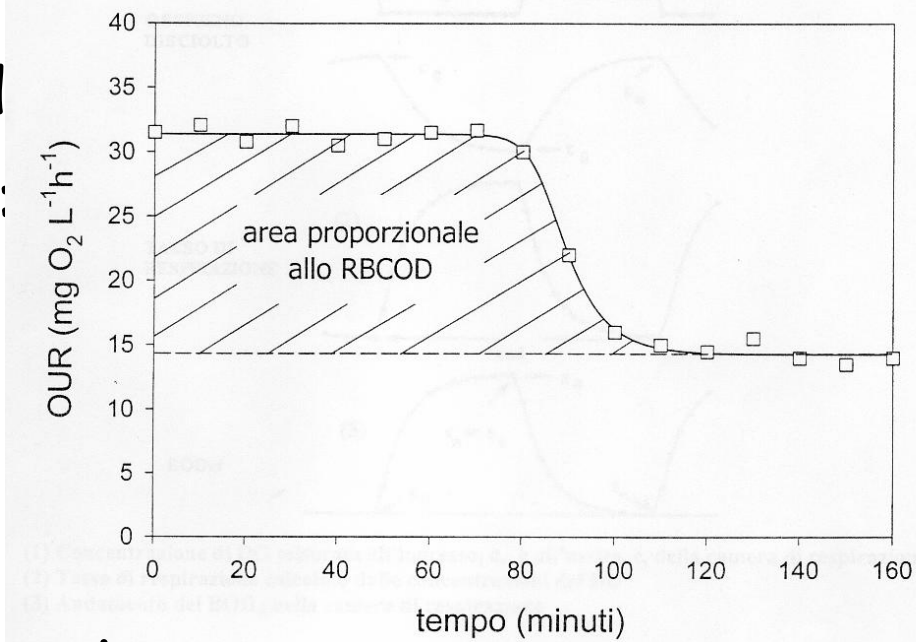
- 1) a wastewater sample is added
- 2)  $r_o$  (OUR) vs time is measured:

3) Oxygen consumed is calculated (dotted area)

$$\Delta O_2 = \int r_o dt$$

4) rbCOD is calculated by subtracting the fraction used for growth

5)  $Y_H$  has been previously calculated with calibration tests, where a known amount of sodium acetate is added, assuming that rbCOD = sodium acetate



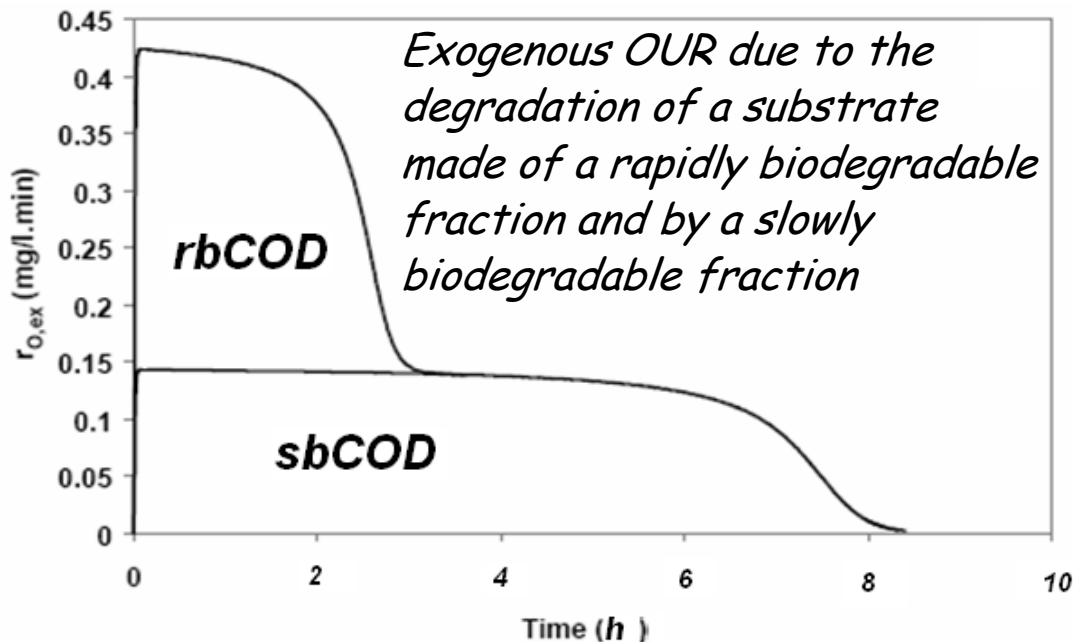
$$rbCOD = \frac{\Delta O_2}{-Y_H}$$



Total biodegradable COD = bCOD = rbCOD + sbCOD

*Test conditions :*

- Biomass concentration: high enough so that  $r_o$  is clearly measurable (0,8-2 gVSS/L)
- F/M ( $bCOD_{ww}/COD_{biomass}$ ) high enough (0,2-0,4) to ensure at least 2 hours at sustained OUR values
- Nitrification is suppressed by ATU addition

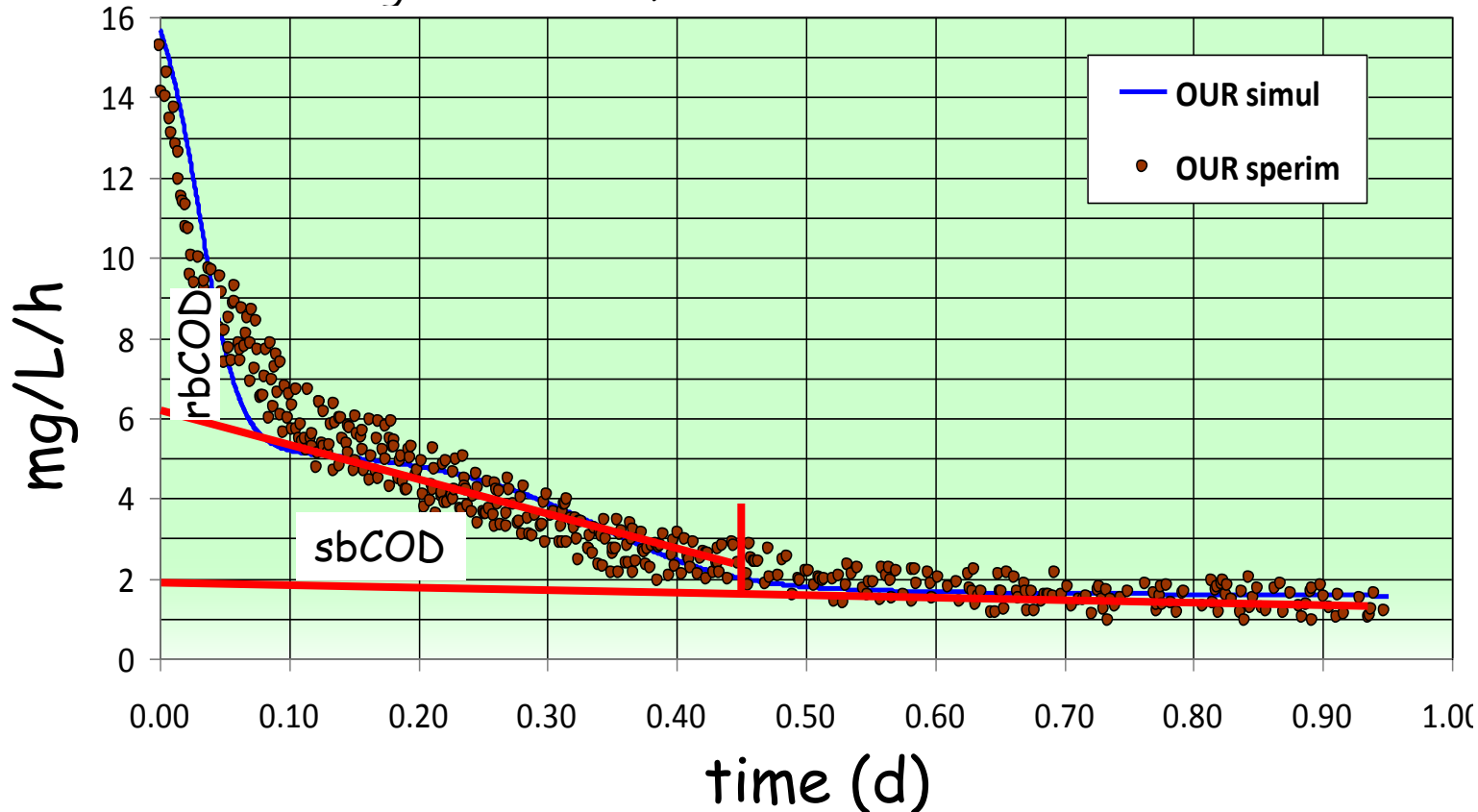




Actual example of an experiment with real sewage

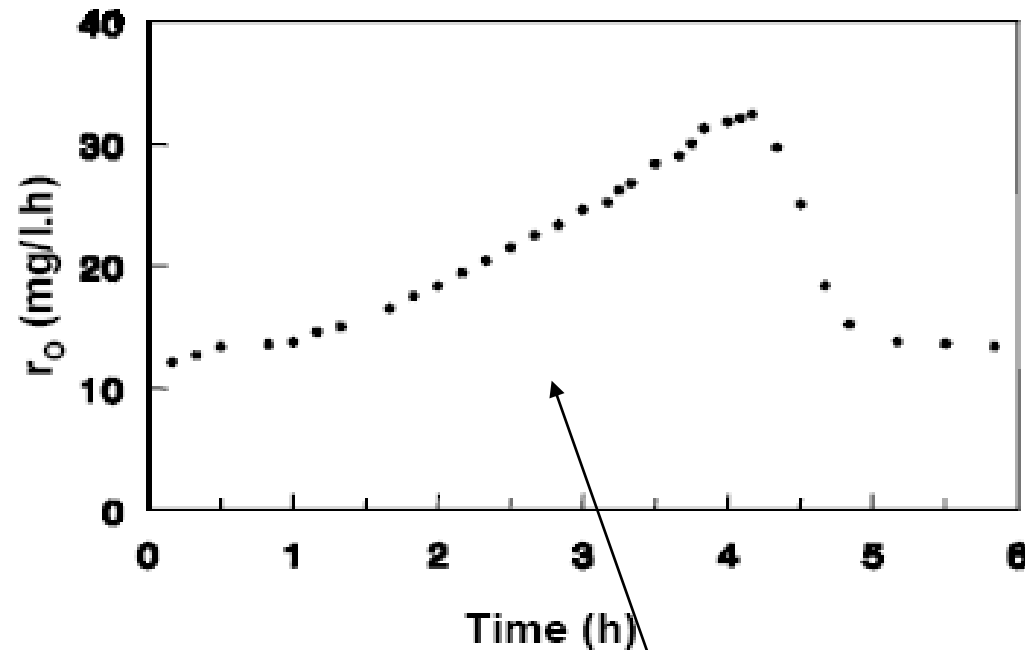
rbCOD is almost absent and sbCOD is made of a mixture of substrates)

*The blue line is an ASM1 simulation of the respirogram : sbCOD and rbCOD have been chosen as the values that give the best fit.*





# Respirometry (12): maximum growth rate ( $\mu_{max}$ ) and active heterotrophic biomass ( $X_{bh}$ ) - 1 16



*Test conditions :*

- High F/M (2-4) so that  $S_s \gg K_s$  and  $X_{bh}$  growth can be observed during the experiment
- Nitrification is suppressed by adding ATU

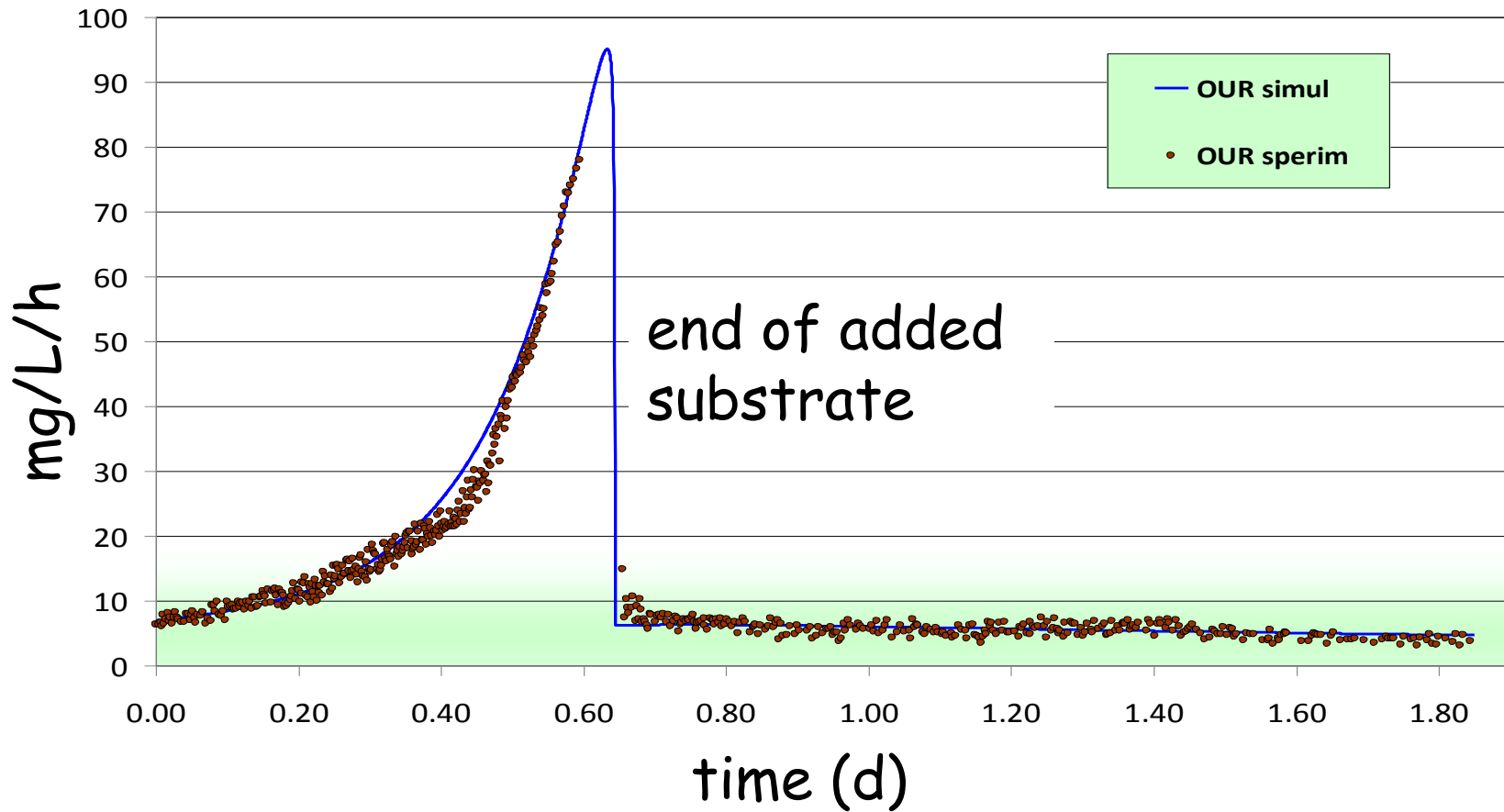
Only data in the exponential growth phase are considered





# Respirometry (13): maximum growth rate ( $\mu_{max}$ ) and active heterotrophic biomass ( $X_{bh}$ ) - 2 17

*Actual experimental test with ASM1 interpretation*



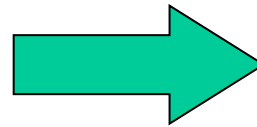


As for Oxygen, it can be written

$$r_O = \frac{1 - Y_H}{Y_H} \cdot \left( \hat{\mu} \cdot \frac{S_S}{S_S + K_S} \cdot \frac{S_O}{S_O + K_{OH}} \right) \cdot X_{BH}$$

As  $S_S \gg K_S$ ,  $S_O \gg K_{OH}$

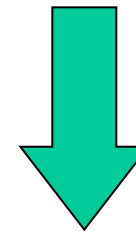
$$\frac{S_S}{S_S + K_S} \cong 1; \quad \frac{S_O}{S_O + K_{OH}} \cong 1$$



$$r_O = \frac{1 - Y_H}{Y_H} \cdot \hat{\mu} \cdot X_{BH}$$

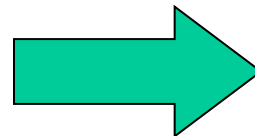
As for biomass, it can be written:

$$r_{X_{BH}} = \frac{dX_{BH}}{dt} = (\hat{\mu} - b) \cdot X_{BH}$$



And, integrating:

$$X_{BH} = X_{BH}(0) \cdot e^{(\hat{\mu} - b)t}$$



$$r_O(t) = r_O(0) \cdot e^{(\hat{\mu} - b)t}$$



$$r_o(t) = r_o(0) \cdot e^{(\hat{\mu} - b) \cdot t}$$

or, in logarithms  $\ln(r_o(t)) = (\hat{\mu} - b) \cdot t + \ln(r_o(0))$

which is a straight line  $y = mx + q$  where:

$$q = \ln(r_o(0)) \quad \text{and} \quad m = \hat{\mu} - b$$

$$x = t, \quad y = \ln(r_o(t))$$

Therefore it can be written 
$$e^q = \left( \frac{1 - Y_H}{Y_H} \hat{\mu} \right) \cdot X_{BH}(0)$$

As  $Y_H$  is known and assuming  $\hat{\mu} \gg b$ ,  $X_{BH}(0)$  can be estimated

$X_{BH}(0)$  = active biomass in the original activated sludge sample



# TITRIMETRY

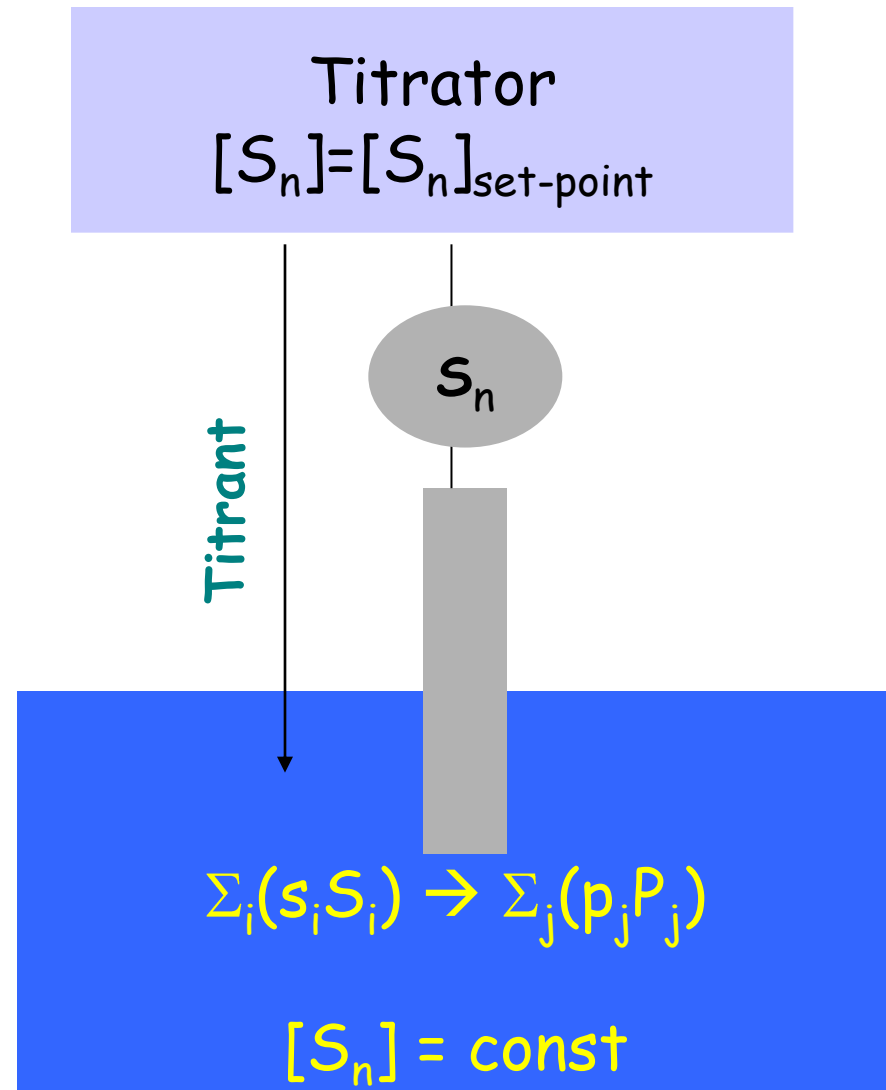


A bioreaction to be monitored takes place in a fed-batch reactor.

A sensor measures the concentration of one among  $S_i$  or  $P_j$  (e.g.  $[S_n]$ ) and a titrator keeps  $[S_n]$  constant by addition of an appropriate titrant.

Normally the titration experiment stops when one of the substrates is used up (e.g.  $S_L$ )

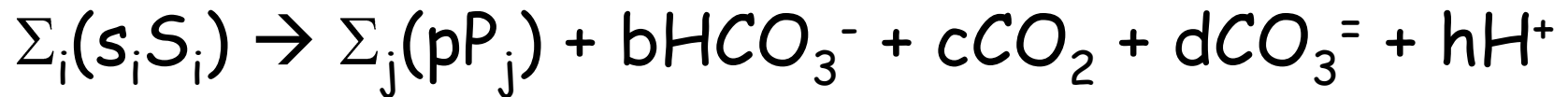
If  $S_n = [H^+] \rightarrow \text{pH} = \text{constant}$





Biomass activity tests with pH-stat titration  
Generic biological reaction **involving protons**

*a) stoichiometry*



*b) reaction rate  $r_{p,i}$  can be measured by the titration rate  $r_t$*

$$r_{p,i} = d[P_i]/dt \propto r_t = r_t(1) + r_t(2)$$

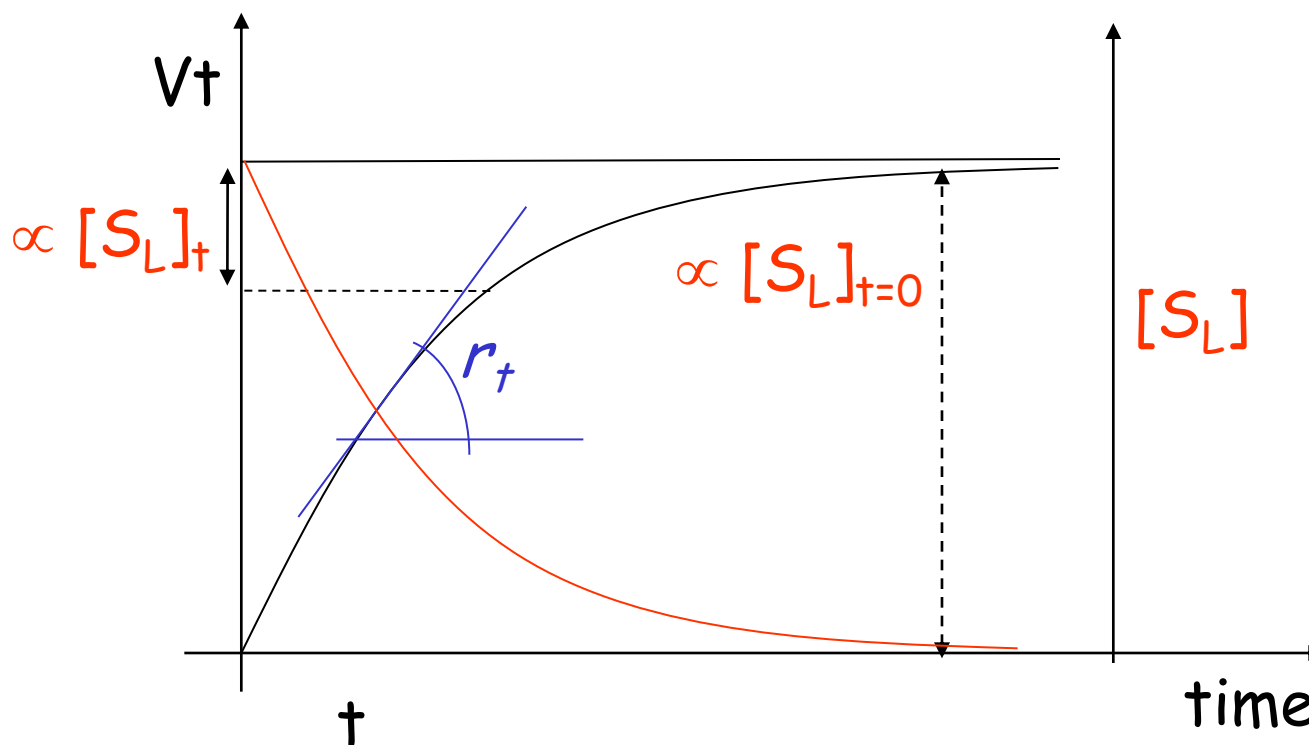
*(1) accounts for products formation;*

*(2) accounts for gas transfer in open systems*



**Titration curve:** volume of titrant added ( $V_t$ ) vs time

**Titration rate:**  $r_t = \frac{dS_n}{dt}$

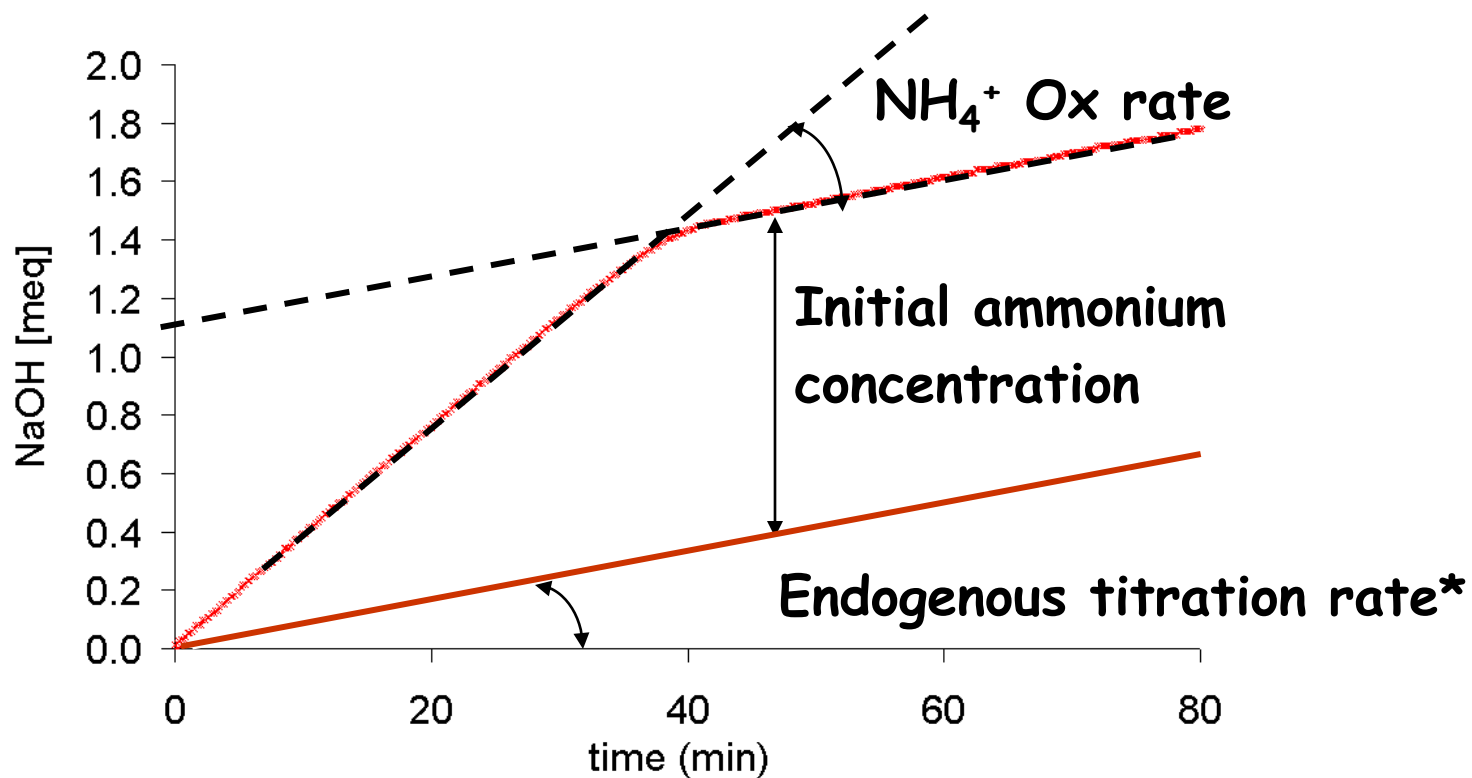




Application of the pH-DO stat titrator to assess:

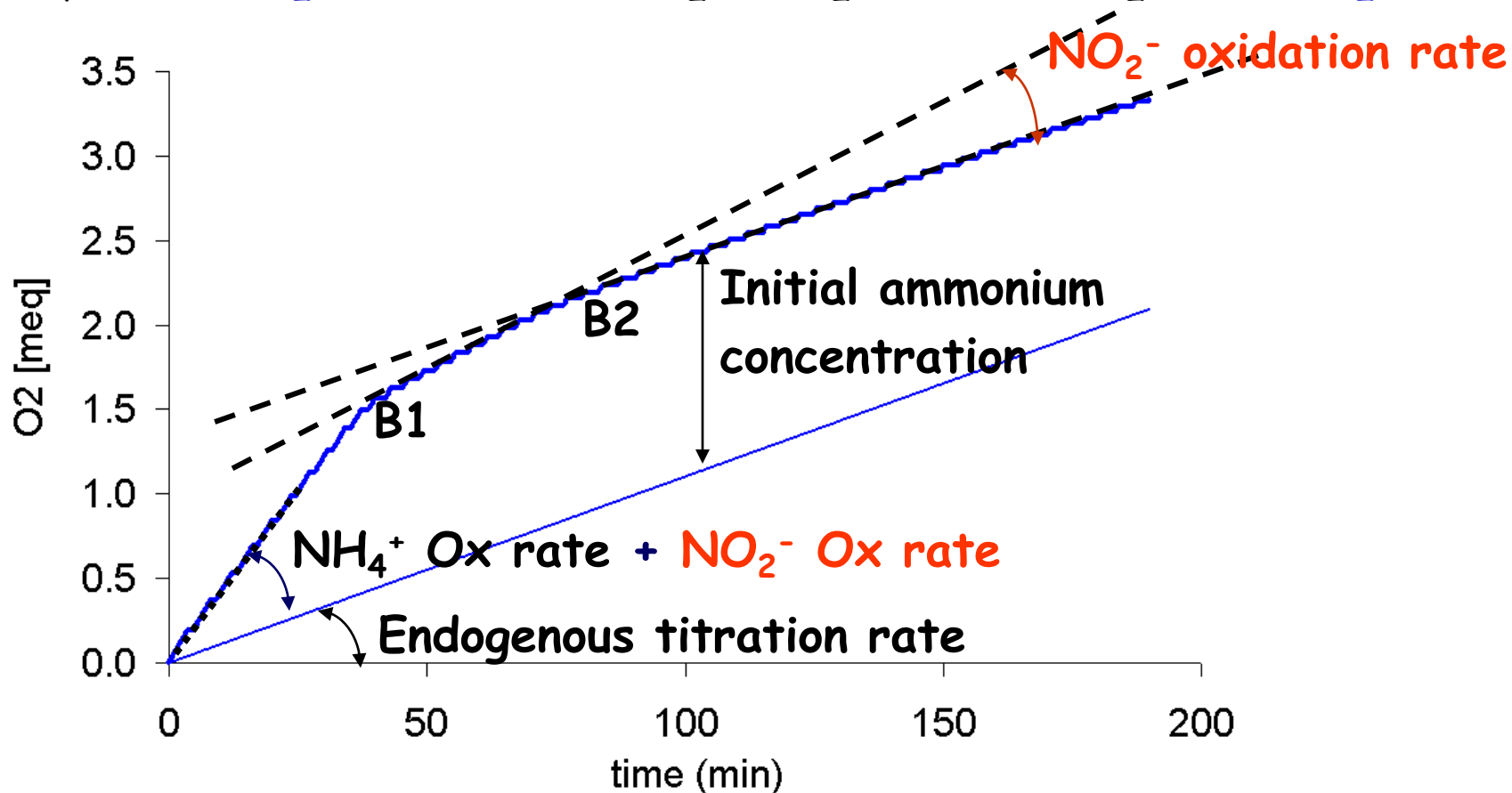
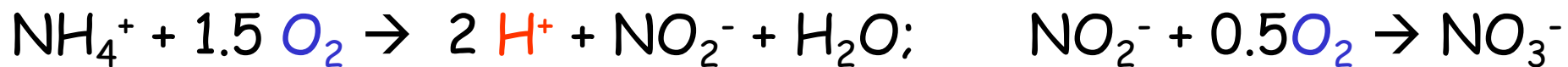
- maximum and actual **nitrification activity**
- detection of the **end of nitrification** during the aeration phase of the SBR cycle
- **denitrification activity** of SBR sludge



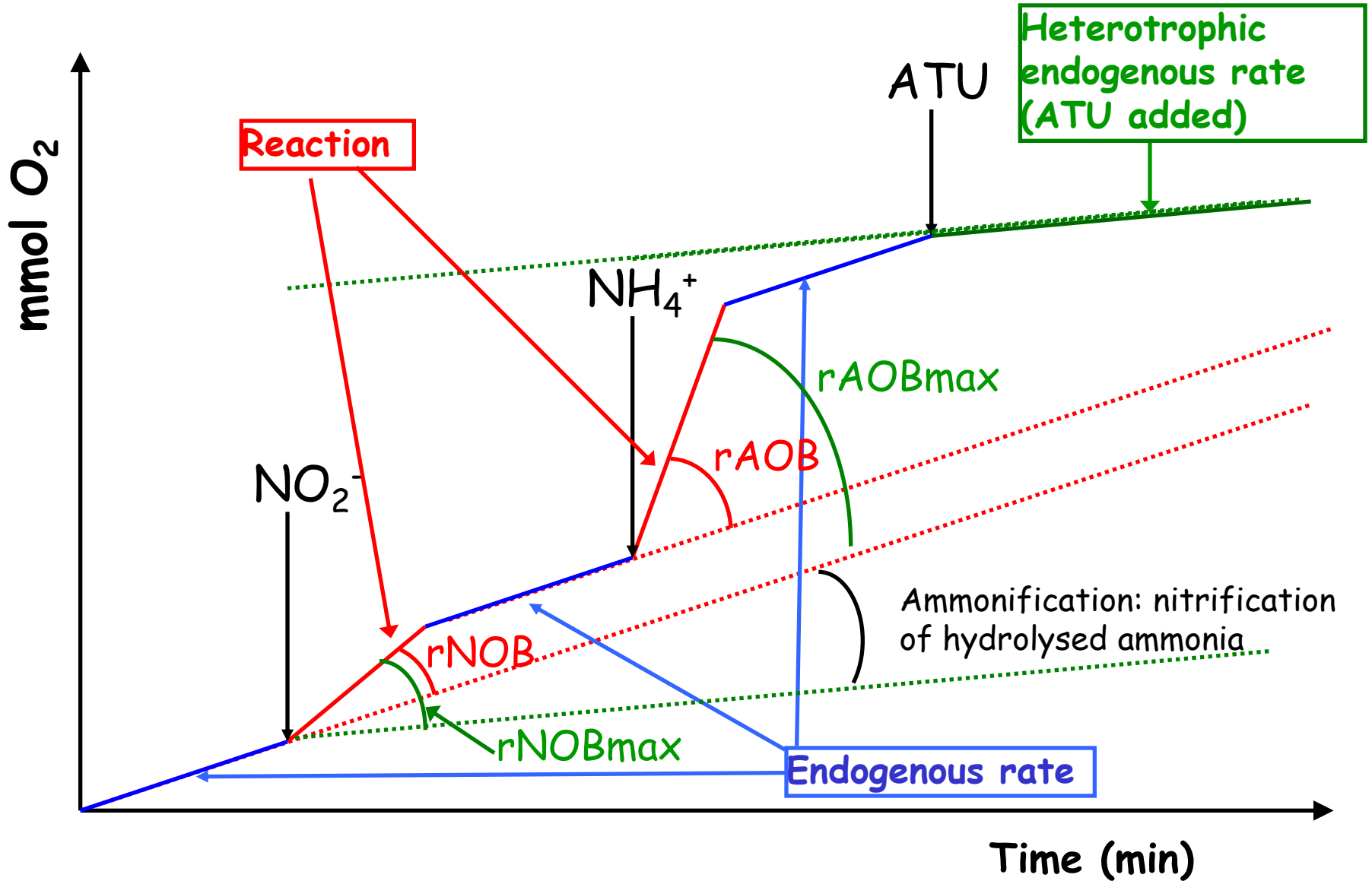


Stoichiometric factor: 2 mol OH<sup>-</sup> = 1 mol NH<sub>4</sub><sup>+</sup>

\* Due to heterotrophic respiration producing CO<sub>2</sub> which absorbs NaOH



Stoichiometric factors:  $1.5 \text{ mol O}_2 = 1 \text{ mol NH}_4^+$   
 $0.5 \text{ mol O}_2 = 1 \text{ mol NO}_2^-$





## Lab- scale SBR (30 L cylindrical tank - working volume 20 L)

aeration system

controlled heating system  $T = 25^{\circ}C$

Online monitoring unit (pH, DO, ORP, T)

peristaltic pumps for effluent discharge

- 1 connected to the floater
- 1 safety pump at the maximum level 20 L

peristaltic pumps for feeding

- 1 for concentrated influent (10X)
- 1 for dilution water



## Titrants:

-NaOH	0.05 M
-H <sub>2</sub> O <sub>2</sub>	0.1 - 0.3 M
-HNO <sub>3</sub>	0.05 M

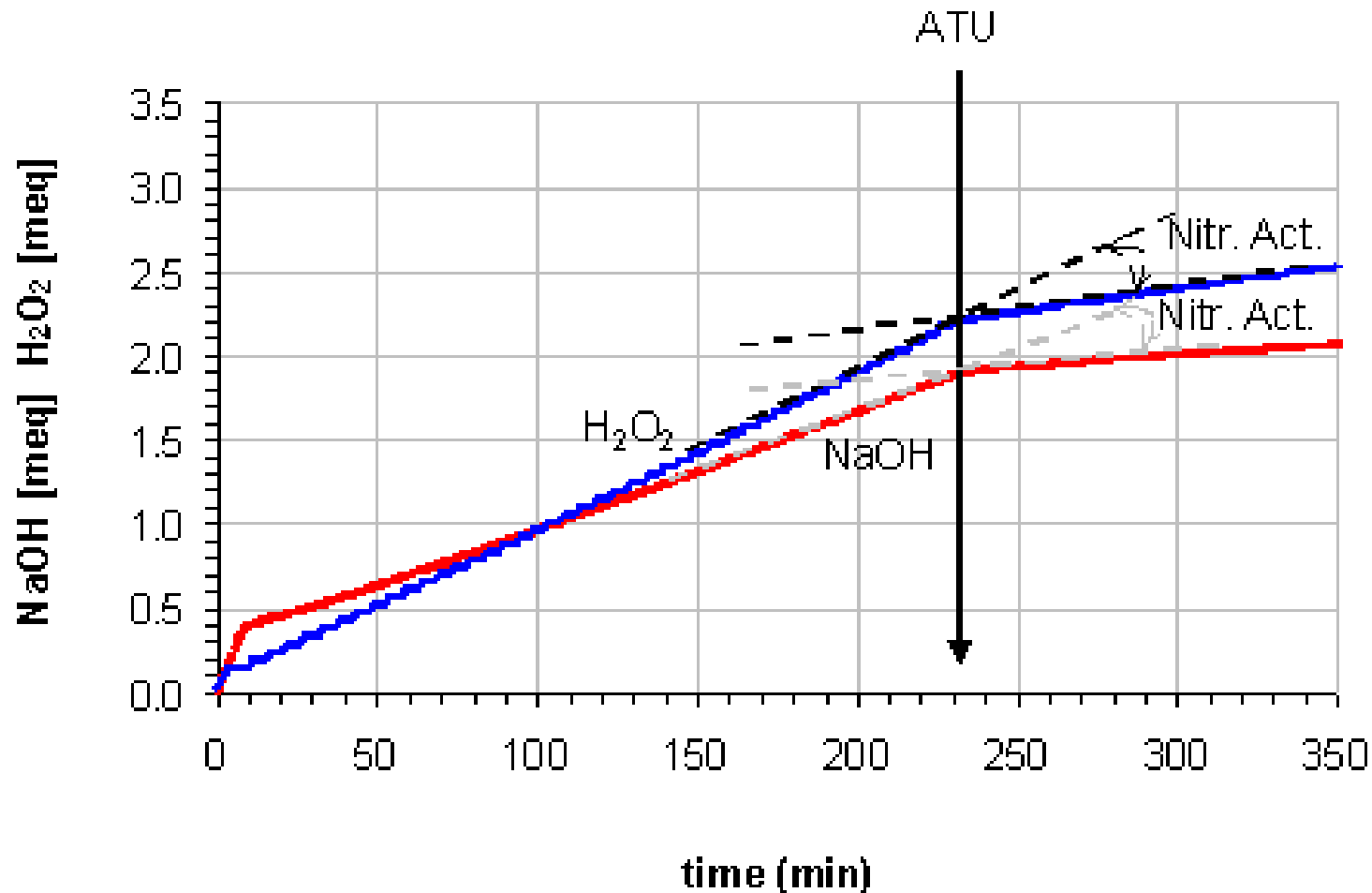
## Set-point values:

-DO<sub>sp</sub> = 8 mg/L  
-pH<sub>sp</sub> = 8.3 } for nitrification tests

(pH<sub>sp</sub> = 7.4 - 7.9 for denitrification tests)

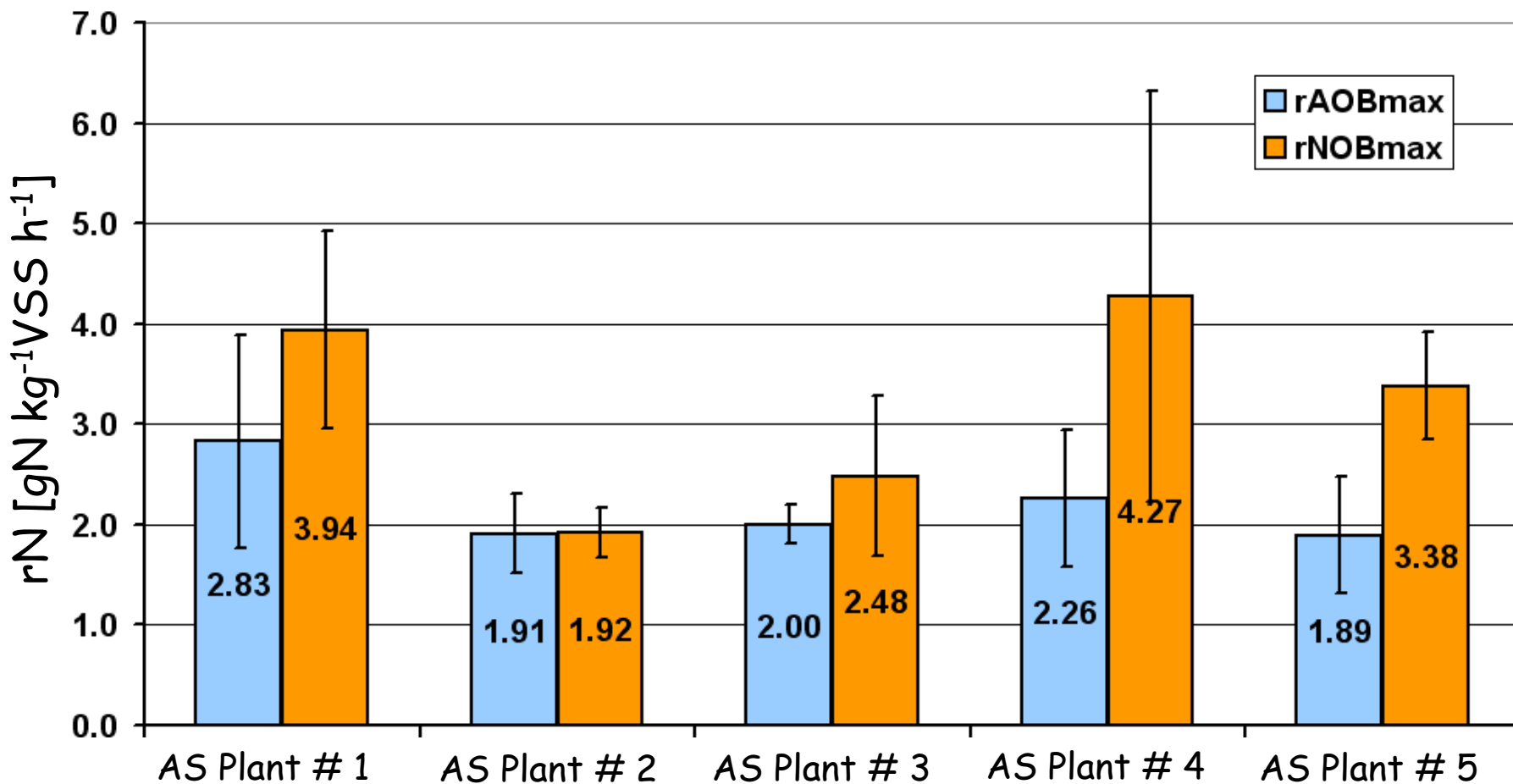


## Real output with freshly sampled activated sludge





## Seasonal monitoring in 5 full-scale WWTPs (activated sludge process)

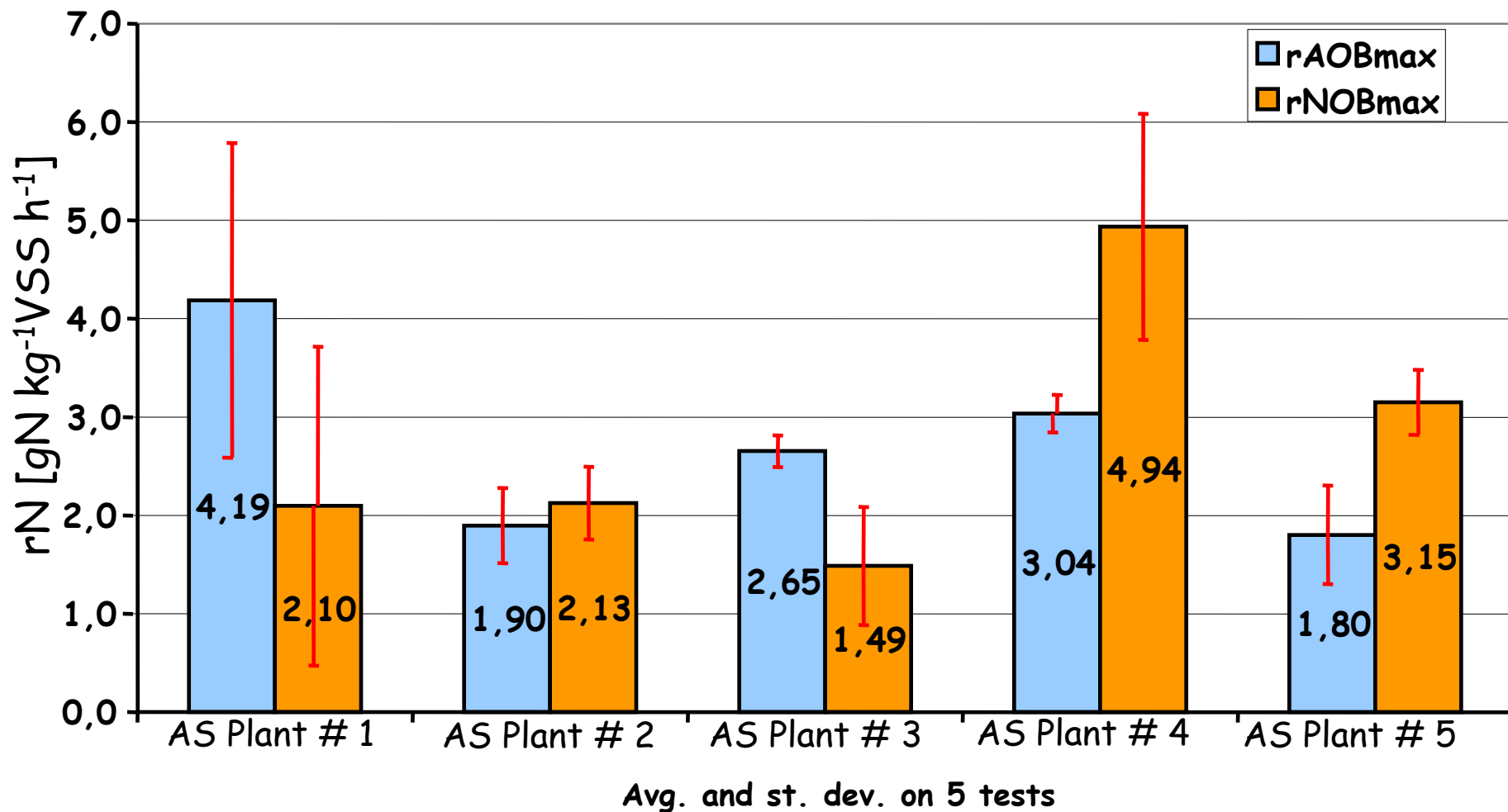


Avg. and st. dev. on 5 tests

All WWTP have  $rAOB_{max} \leq rNOB_{max}$ , i.e.: no nitrite build-up



## Seasonal monitoring in 5 full-scale WWTPs (activated sludge process)



WWTP #1 and 3 have rAOBmax > rNOBmax, i.e.: risk of nitrite build-up

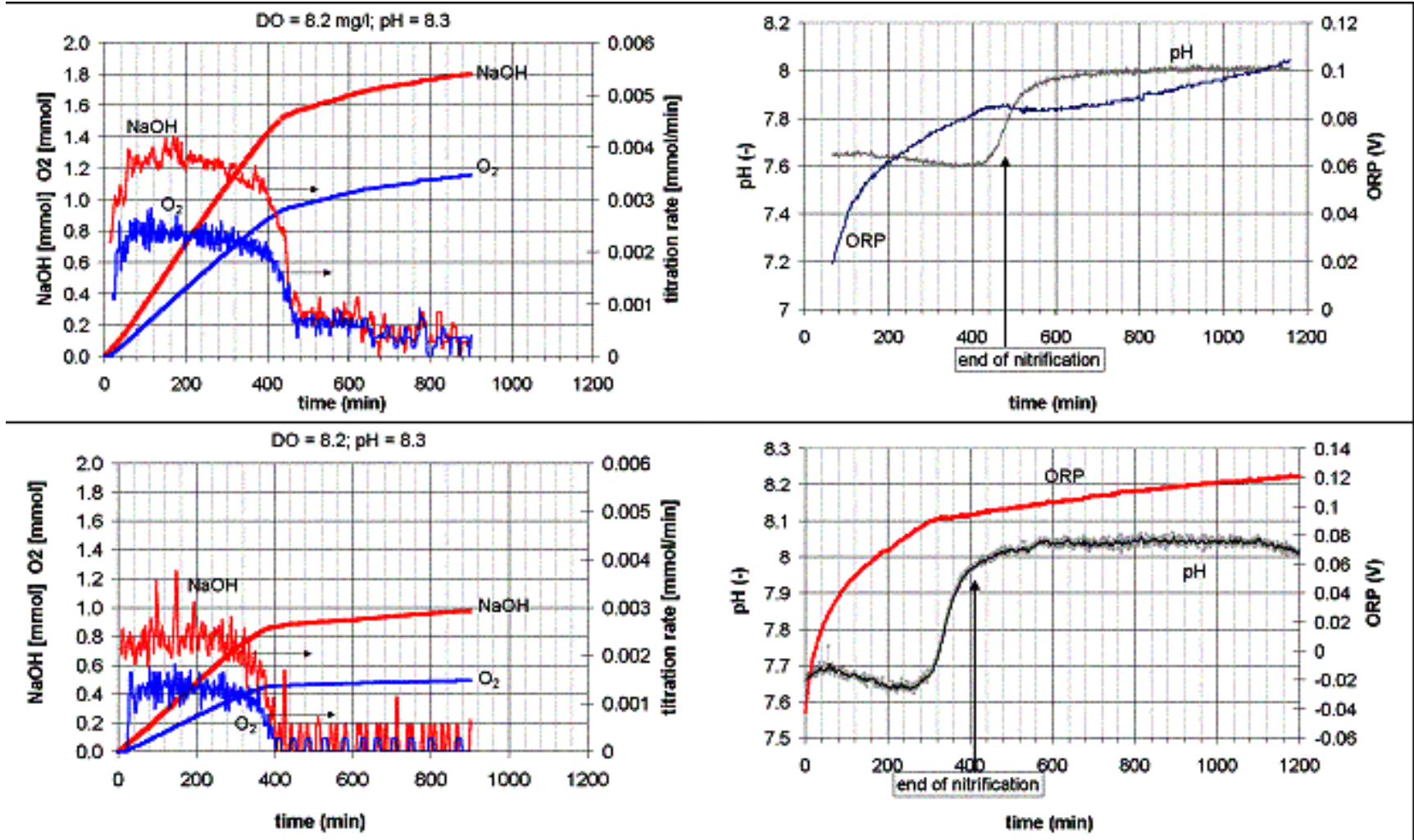




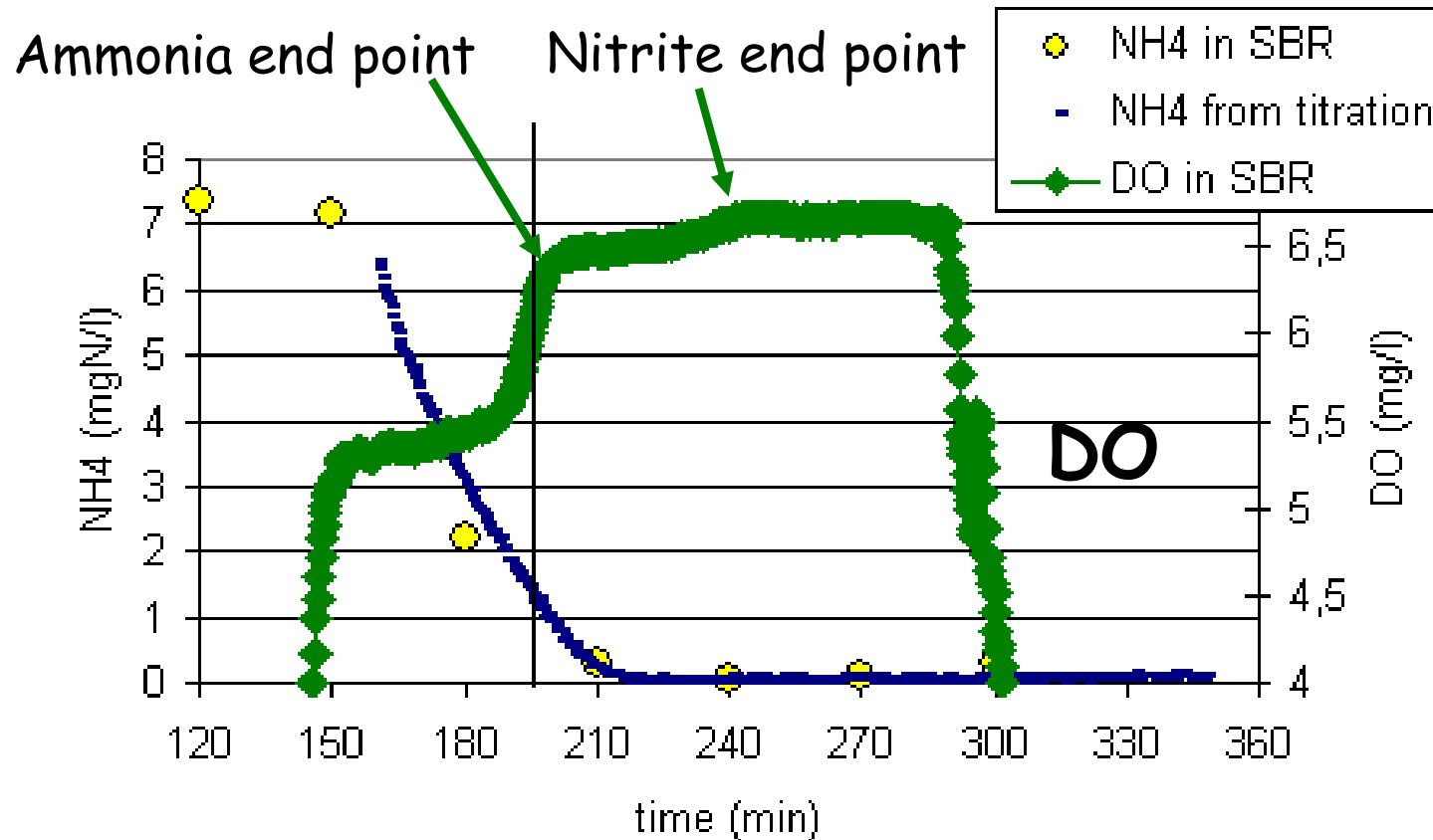
Martina

vs.

SBR

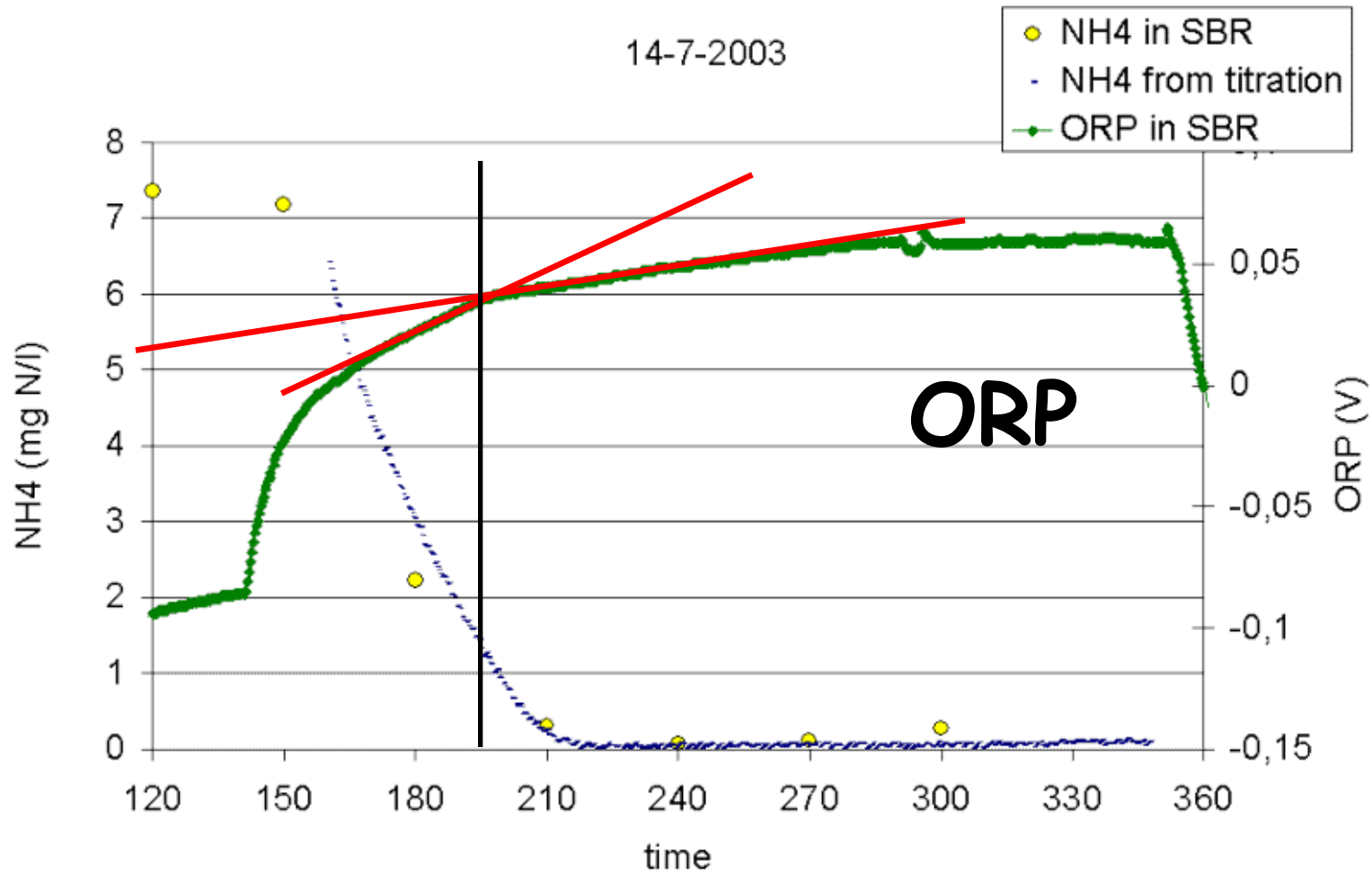


## Comparison between Lab-Titrator (Martina) and SBR

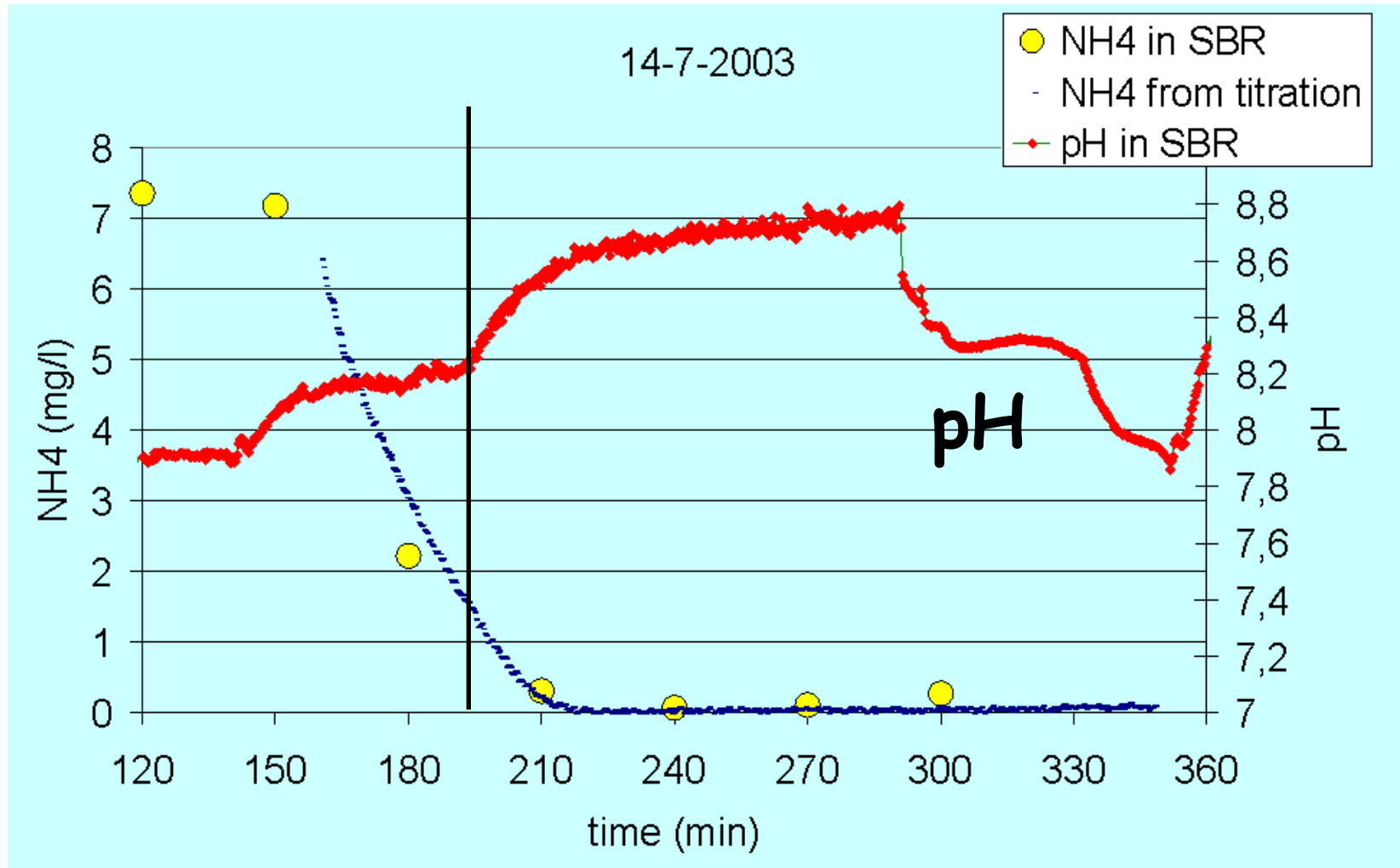




## Comparison between Martina and SBR - ORP

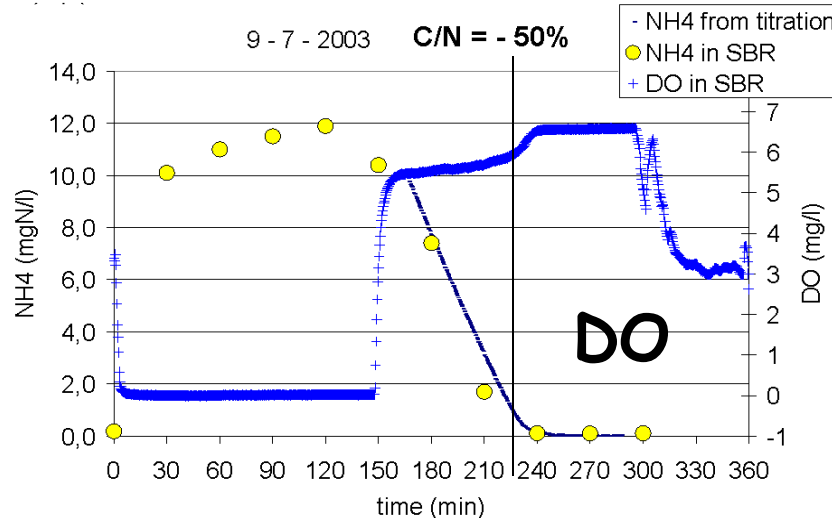
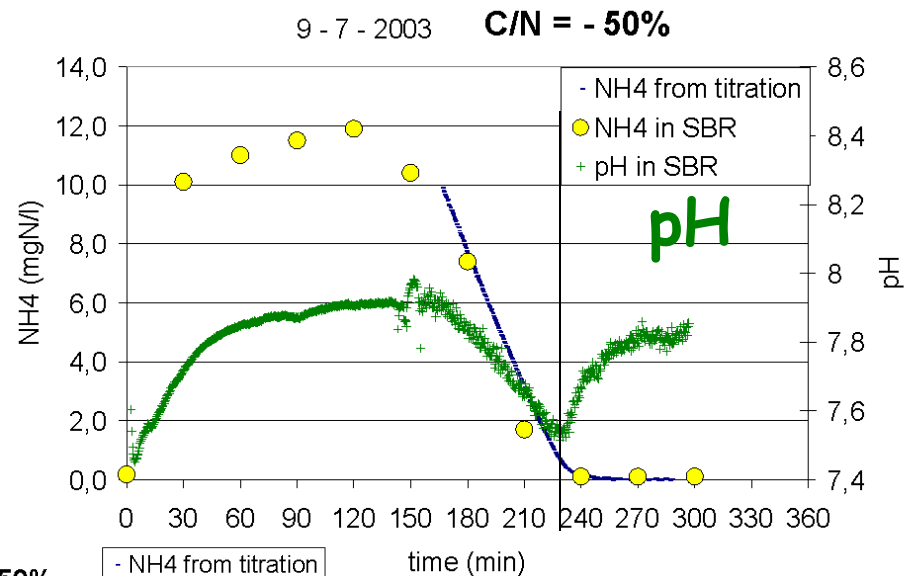
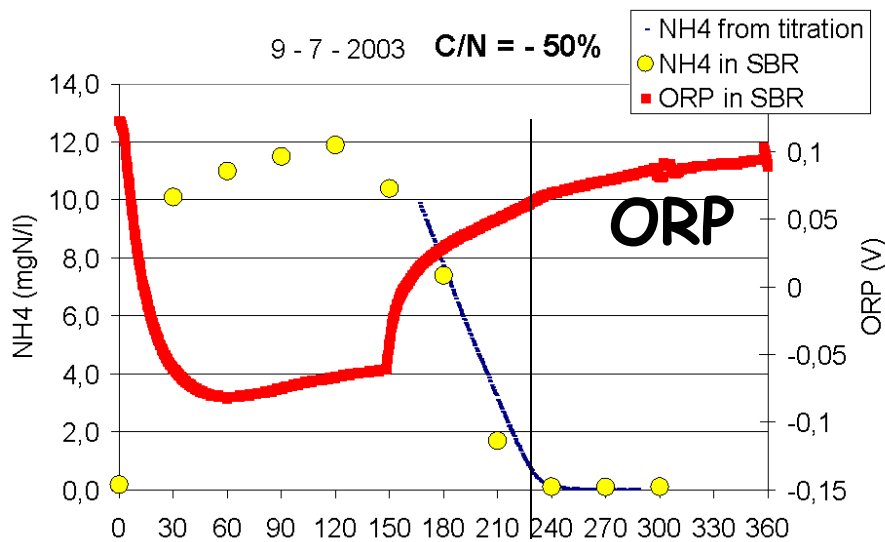


## Comparison between Martina and SBR

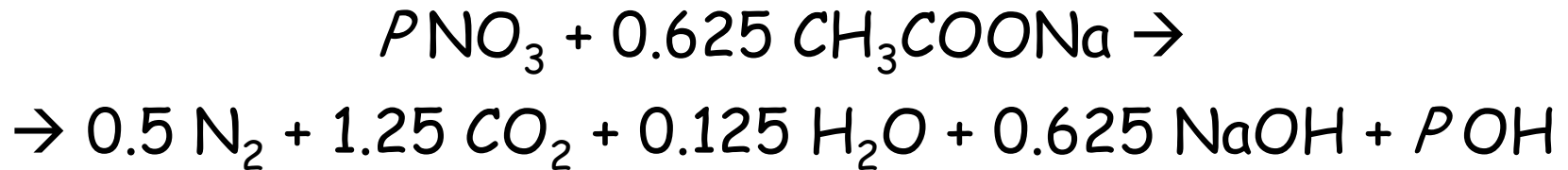




## Comparison between Martina and SBR



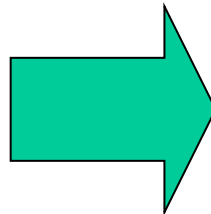
## Heterotrophic denitrification activity tests with pH-stat titration



$P$  cation ( $P^+$ ) not influencing pH (i.e.:  $Na^+$ )

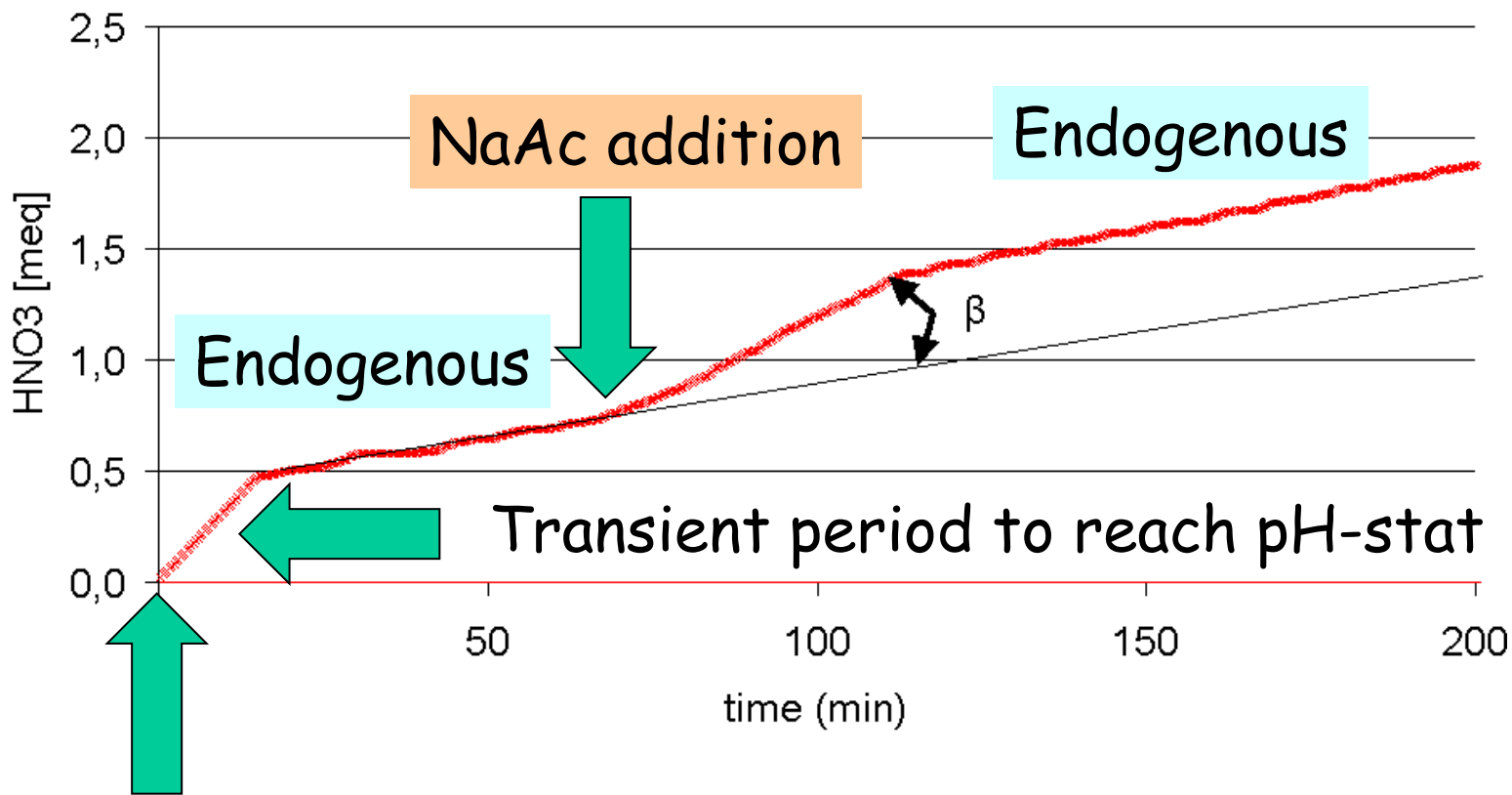
$CH_3COONa$   
as carbon source

$HNO_3$   
Titrant



COD-limited reaction  
 $NO_3^-$  not limiting

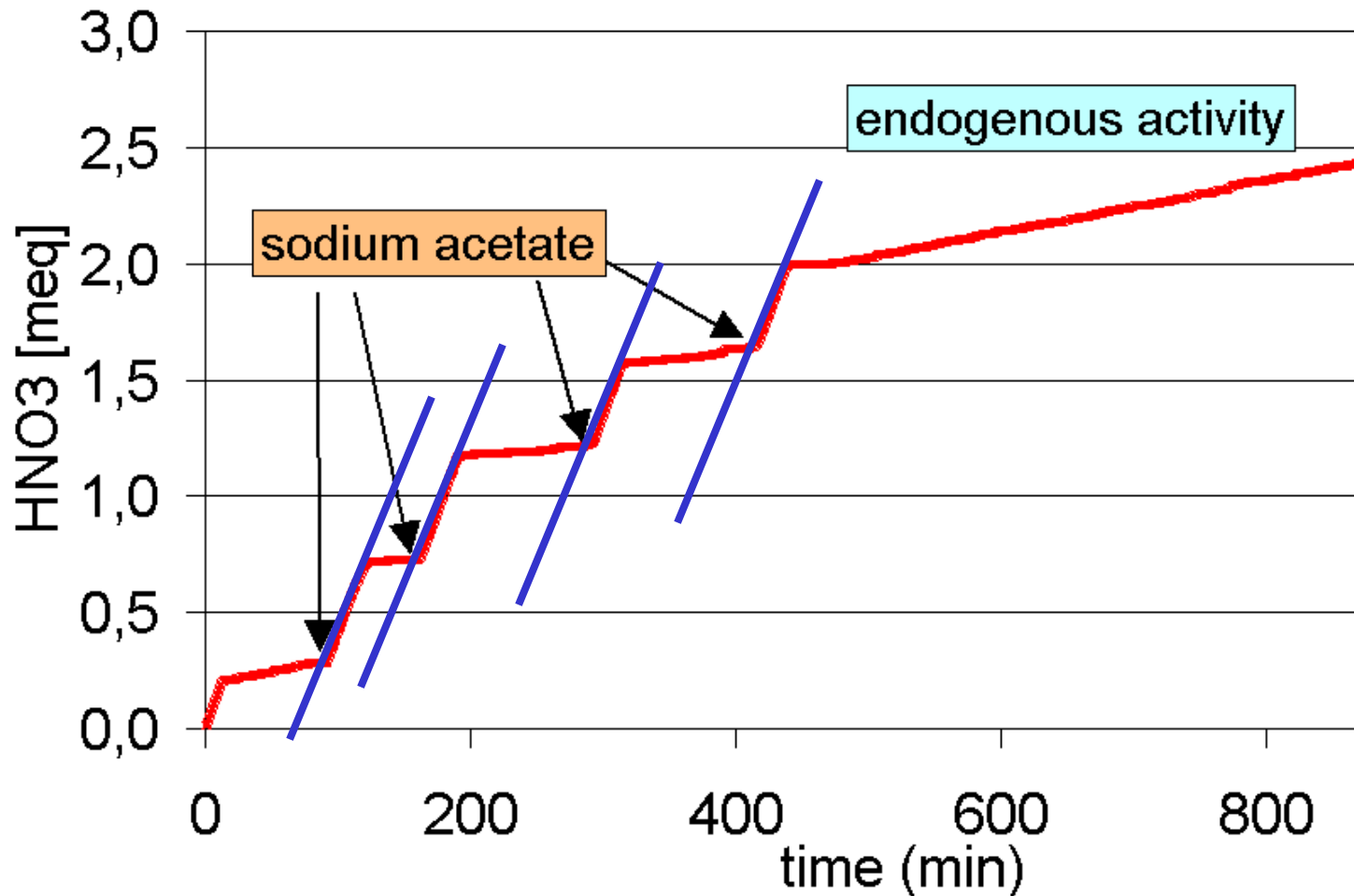
# Denitrification activity tests with acetate



Nitrate 60 mgNO<sub>3</sub><sup>-</sup>/L (13,5 mg/L as N)

# Denitrification activity tests with acetate

## Tests are fully repeatable





## Denitrification activity tests with acetate

Run n°	denitrification rate [mgN -NO <sub>3</sub> /gVSS*h]
1	12,68
2	15,95
3	18,68
4	19,76
5	17,50
6	17,58
7	20,35
8	19,97

Max denitrification rate: 20 mgN-NO<sub>3</sub><sup>-</sup> g<sup>-1</sup>VSS h<sup>-1</sup>

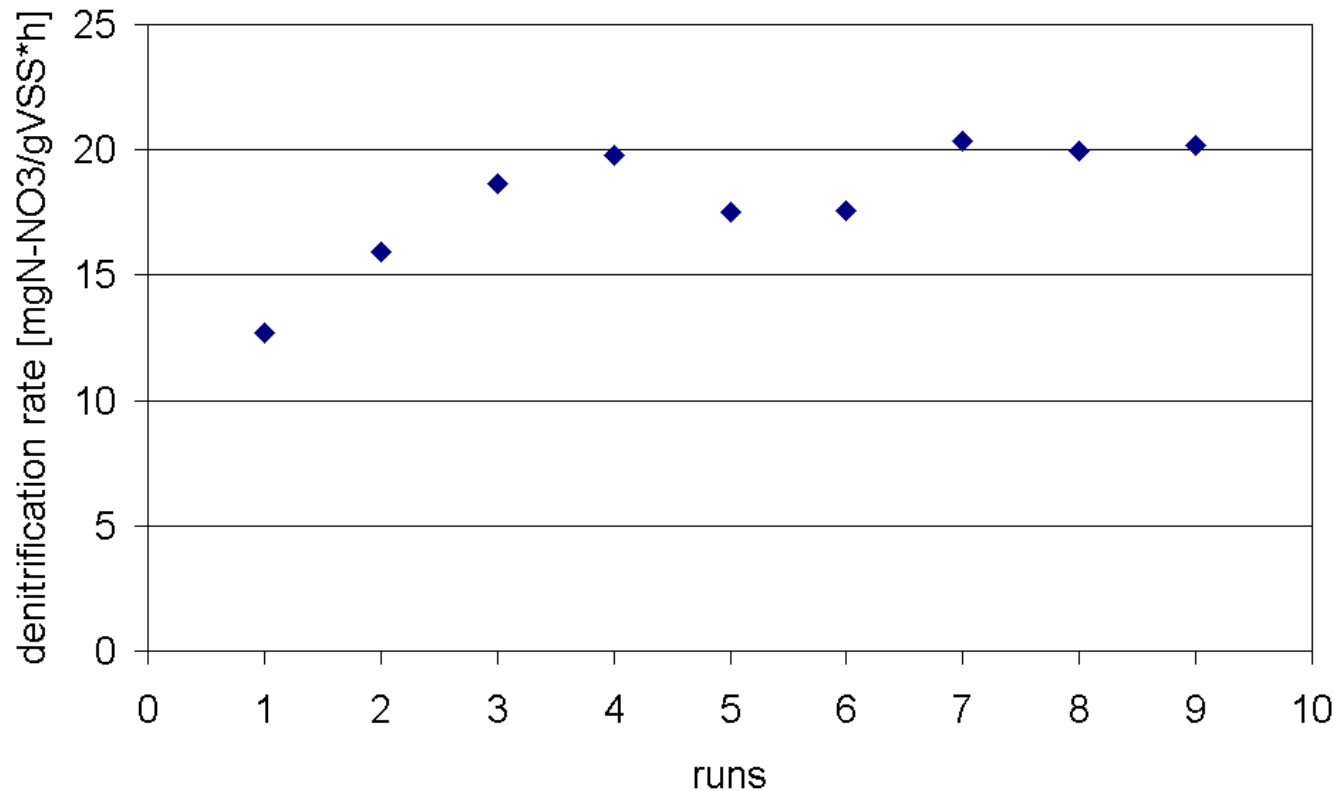
Endogenous rate: 1.12 - 1.94 mgN-NO<sub>3</sub><sup>-</sup> g<sup>-1</sup>VSS h<sup>-1</sup>

(biomass grown on synthetic sewage, high % active biomass, low particulate organic debris)



## Denitrification activity tests with acetate

Denitrifying activity in SBR increased in the first 4 tests (confirmed by nitrate analysis)





# Titrimetry (23) - TITAN (TITrimetric Automated Analyzer - 1)

Sludge+Influent storing tanks

Probes pH/DO (ORP, T)

Titration reactor

Pump +EV for titrant dosage

Titrant tanks

User interface





## Titration MODEs for the assessment of:

1. Acute toxicity of autotrophic biomass
2. Nitrifiable nitrogen in the influent
3. Maximum nitrifying activity
4. End of nitrification process (SBR only)
5. Residual nitrates at end of anoxic/aerobic phase



File in analisi C:\Archivio\Installazioni\2008 Titaan ImolaSanterno\Dati\T1\_20090108\_115121\T1\_20090108\_115121.xls

Dati

Volume Fango [L]

Conc. Fango

Titolo NaOH [mmol/mL]

Titolo H2O2 [mmol/mL]

Elettrovalvola EV 1

Elettrovalvola EV 2

T.Rif.=T.Media [°C]

Vol. Inoculo [mL]

	EndoglNI	Nitrif	EndogFIN	Gin. [min]
NaOH	<input type="text"/>	29.65	6.14	42
i.c.95%	<input type="text"/>	0.01%	0.02%	1
H2O2	<input type="text"/>	24.69	11.05	42
i.c.95%	<input type="text"/>	0.01%	0.02%	3

Attività

	mgN / (L*h)	mgN / (gSSV*h)	Errore
AOB	8.2	2.4	0.98%
NOB	0	0	
AOB_NOB	4.8	1.4	0.96%

Intervalli [mm:ss]

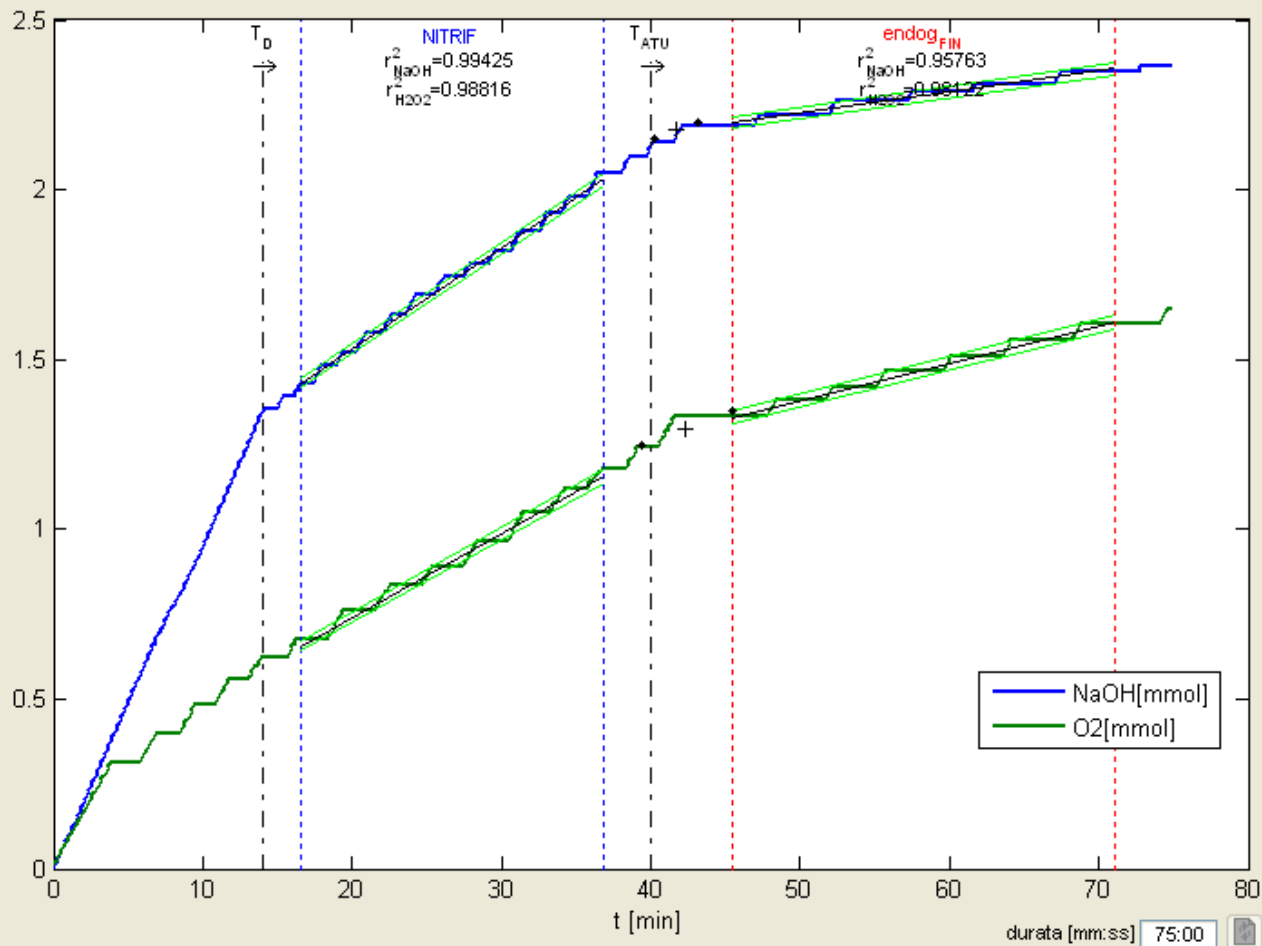
end. iniziale

tD

Attività nitrificante

tATU

end. finale



durata [mm:ss]

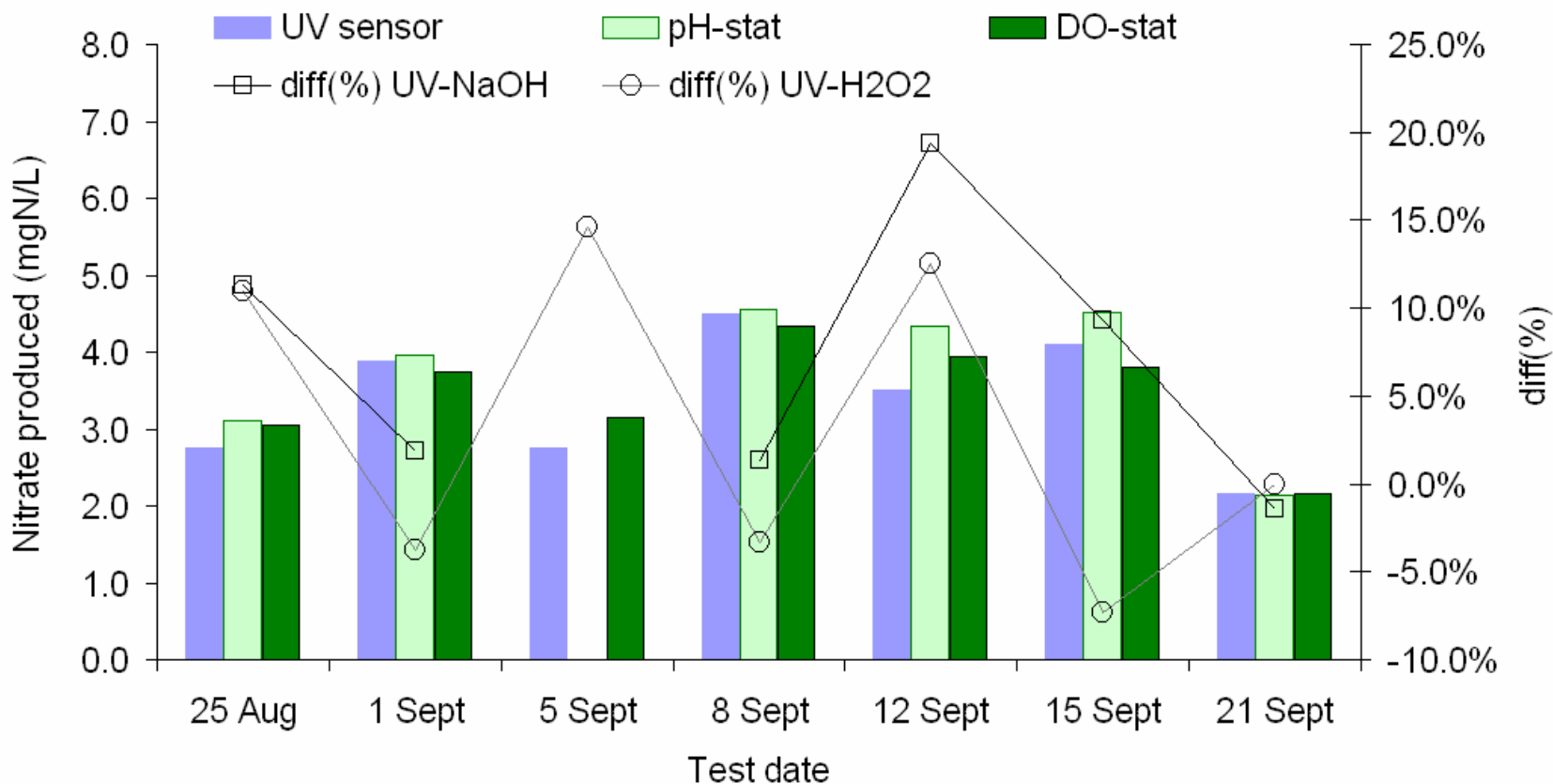


## On-line nitrification activity data validation in SBR:

Production of  $\text{N-NO}_3^-$  during aerobic phase

1) estimated on-line by TITAAN-Mode 1 pHstat and DOstat

2) measured by on-line UV sensor and validated with lab analysis (LPI C)



**satisfactory correspondence: avg. error 8%**