

Reduction of the ADM1 model

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 - is a high order nonlinear model, not suited for control design.
- Model reduction techniques appear as appropriate tools for obtaining reduced order linear or nonlinear models.

Simplification of the kinetics equations

- Monod growth rate expression:

$$\mu(S) = \mu_{\max} \frac{S}{S + K_S}$$

μ_{\max} → The maximum growth rate (1/day)

K_S → The half-saturation constant (gCOD/L)

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- Blackman growth rate expression:

$$\mu(S) = \begin{cases} \frac{\mu_{\max}}{K_S} S & \text{if } S \leq K_S \\ \mu_{\max} & \text{if } S > K_S \end{cases}$$

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- We assume that it is enough to suit our objectives by neglecting all chemical or physicochemical phenomena.
- We remove the state variables whose dynamics are uncoupled from other components:
 - Soluble inert component S_j
 - Particulate inert component X_j

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- Implies starting with a system in which the relation eigenvalues-states is obvious such as a decoupled system or a diagonalised matrix A . The transformation is described by the equation:



$$H(r) = (1 - r).A_D + r.A \quad 0 \leq r \leq 1$$

- H Homotopy matrix

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- r a parameter that allows to obtain a linear progression from the decoupled system to the coupled one

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- It is assumed that the system admits at least one equilibrium point locally asymptotically stable
- The homotopy method is applied to a stable equilibrium point of the differential system (11 differential equations for the soluble components, 11 for the particulate ones)

Simulation results

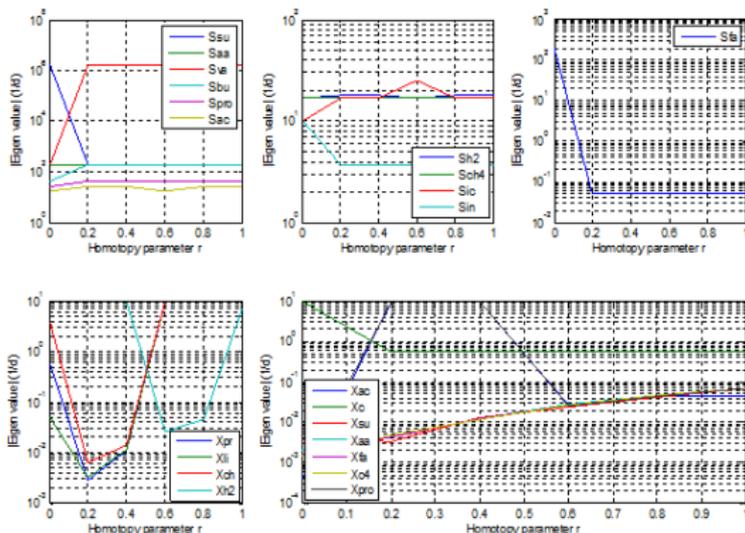


Figure 1 - Results of the homotopy method on the fast and slow variables

State variables	Eigenvalues (1/d)	$\tau(h)$
S_{va}	-1585389, 931	0, 00002
S_{aa}	-200, 050	0, 119
S_{su}	-200, 049	0, 119
S_{bu}	-196, 449	0, 122
S_{pro}	-40, 870	0, 587
S_{ac}	-25, 162	0, 953
S_{h2}	-17, 832	1, 345
S_{ch4}	-16, 993	1, 412
S_{ic}	-16, 924	1, 418
X_{pr}	-10, 050	2, 388
X_{li}	-10, 050	2, 388
X_{ch}	-10, 049	2, 388
X_{h2}	-7, 002	3, 427
S_{in}	-3, 636	6, 600

State variables	Eigenvalues (1/d)	$\tau(h)$
X_c	-0,552	43,456
X_{aa}	-0,070	341,491
X_{fa}	-0,070	342,514
X_{c4}	-0,070	342,514
X_{pro}	-0,069	342,906
X_{su}	-0,068	352,319
S_{fa}	-0,050	480,000
X_{ac}	-0,045	527,588

Table 3 - Eigenvalue and time constant association

- The differential system is reduced to 14 differential equations represented by the following state variables: S_{su} , S_{aa} , S_{va} , S_{bu} , S_{pro} , S_{ac} , S_{h2} , S_{ch4} , S_{ic} , S_{in} , X_{ch} , X_{pr} , X_{li} , X_{h2} other variables being considered as constants.

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- The reduced model keeps the particulate components X_{ch} , X_{pr} , X_{li} which are the most important particulate substrates identified by the ADM1 model (Batstone et al., 2002).

The case study

- A CSTR anaerobic digester fed on waste activated sludge operating under mesophilic temperature.

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- Simulations were performed by using DYMOLA (DYnamic MOdeling LABoratory) to compare the values assumed by the state variables at steady state as predicted by the ADM1 model and by the reduced model

Simulation results

State variables	ADM1 Model	Reduced Model	Relative error (%)
Ssu	0,011	0,019	72,72
Saa	0,0053	0,0050	5,66
Sva	0,011	0,009	18,18
Sbu	0,0132	0,0136	3,03
Spro	0,0157	0,0152	3,18
Sac	0,197	0,024	87,81
Sh2	2,359e-7	2,277e-7	3,48
Sch4	0,0549	0,0544	0,91
Sic	0,152	0,147	3,28
Sin	0,130	0,122	6,15
Xch	0,027	0,024	11,11

State variables	ADM1 Model	Reduced Model	Relative error (%)
Xpr	0,102	0,099	2,94
Xli	0,029	0,024	17,24
Xh2	0,317	0,296	6,62

Table 4 - Steady state values reached by the two models

State variables	ADM1 Model	Reduced Model	Relative error (%)
Sgas CH ₄	1,621	1,618	0,18
Sgas CO ₂	0,014	0,014	0
q gas CH ₄	1709,300	1596,040	6,63
q gas CO ₂	952,399	885,347	7,04

Table 5 - Steady state values for CH₄, CO₂ and their flow rate

A disturbance around the steady state conditions

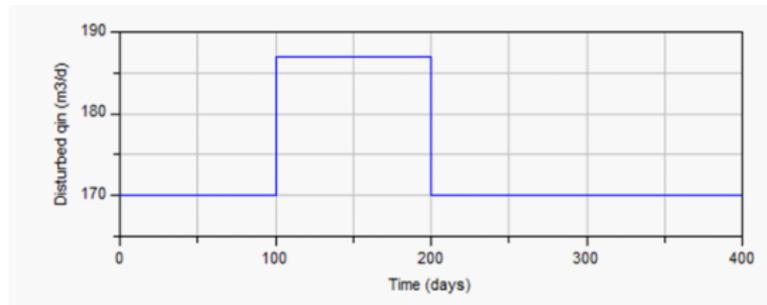


Figure 2 - Step disturbance applied to q_{in}

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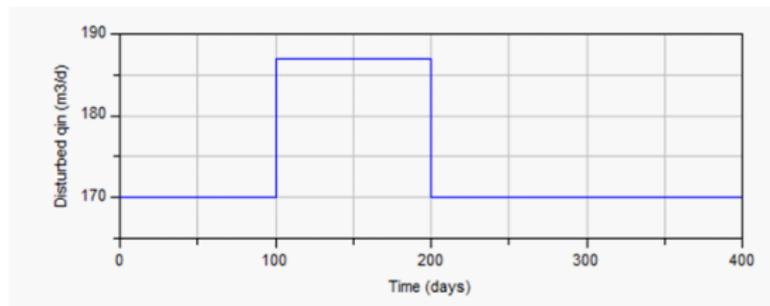
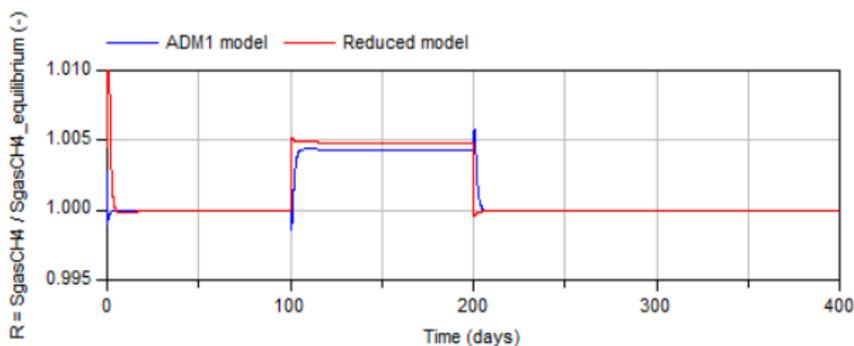
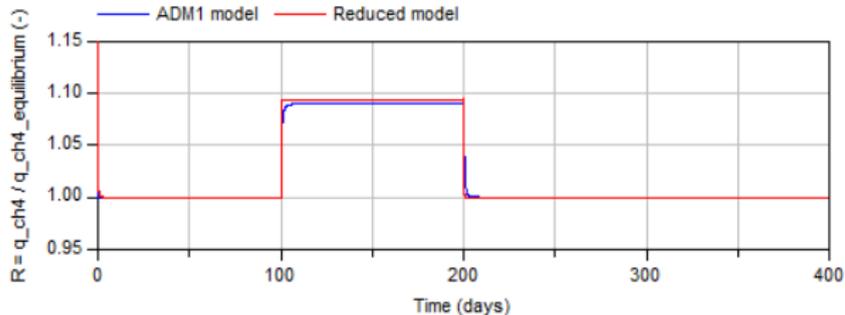


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- A-dimensional ratio R :

$$R_{\text{state variable}} = \frac{\text{State variable } (t)}{\text{State variable } (eq)}$$



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$$\delta_{ij} = \frac{p_i}{y_j(p_i)} \cdot \frac{y_j(p_i + \Delta p_i) - y_j(p_i)}{\Delta p_i} \cdot 100$$

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- For each parameter p_i an absolute variation of 20% of the default value was applied

	$k_{hyd,ch}$	$k_{hyd,pr}$	$k_{hyd,li}$	$k_{dec,Xh2}$	$k_{m,rs}$	$k_{e,rs}$	$k_{m,sa}$	$k_{e,sa}$	$k_{m,ct}$	$k_{e,ct}$	$k_{m,pro}$	$k_{e,pro}$	$k_{m,sc}$	$k_{e,sc}$	$k_{m,h2}$	$k_{e,h2}$
Ssu	1		1		3	3										
Ssu_red	1		1		3	3										
Ssa		1					3	3								
Ssa_red		1					3	3								
Sva							1	1	3	3						
Sva_red							1	1	3	3						
Sbu					1	1	1	1	3	3						
Sbu_red					1	1	1	1	3	3						
Spro					1	1	1	1	1	3	3					
Spro_red					1	1	1	1	1	3	3					
Sac					1	1	1	1	1	1	1	3	3			
Sac_red					1	1	1	1	1	1	1	3	3			
Sh2					1	1	1	1	1	1	1				3	3
Sh2_red					1	1	1	1	1	1	1				3	3
Sch4													1	1	1	1
Sch4_red													1	1	1	1
Sic	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1
Sic_red	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1
Sin				1	1	1	1	1	1	1	1	1	1	1	1	1
Sin_red				1	1	1	1	1	1	1	1	1	1	1	1	1
Xch	3															
Xch_red	3															
Xpr		3														
Xpr_red		3														
Xli			3													
Xli_red			3													
Xh2				2											1	1
Xh2_red				2											1	1

Table 4 - Results of the sensitivity study

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- $2 = 30\% \leq \delta_{ij} \leq 60\%$

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- $1 = \delta_{ij} < 30\%$
- $2 = 30\% \leq \delta_{ij} \leq 60\%$
- $3 = \delta_{ij} > 60\%$
- The sensitivities of the states with regard to the parameters are preserved in the reduced model

- We have implemented the Homotopy method for the reduction of the order of the ADM1 model

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	ADM1 Model	Reduced Model
State variables	24	14
Biomasses	7	1
Parameters	55	40

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- To use the reduced model for control synthesis and apply this controller to the ADM1 model

THANK YOU!